

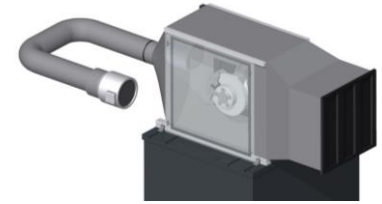


CFD based Analysis of Particle-Air Interaction within a Sampling Device for Brake Dust Emissions

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1. Motivation



Main requirement for a sampling system:

- Providing a representative sample for PN/PM-measurement (PM2.5, PM10)

Implementation by (Homologation):

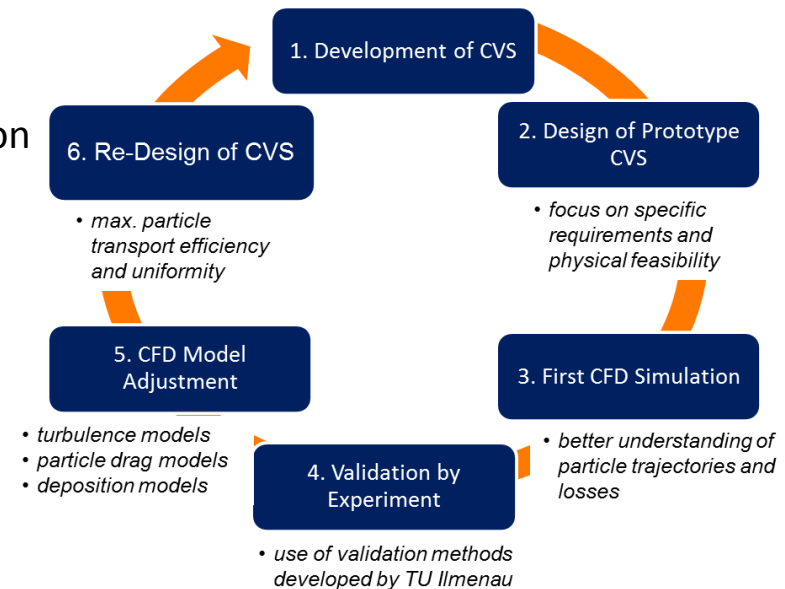
- High sampling- and transport efficiency
- High uniformity of number concentration
- High reproducibility (uniformity, const. Aerosol flow)
- minimizing background concentration (filter)

Influence variables (extract):

- complex geometries → complex flow
- Transport mechanism (external processes)
- injection / initial conditions
- varying parameters over the cycle (rot. speed)
- Disc ventilation

Methodology:

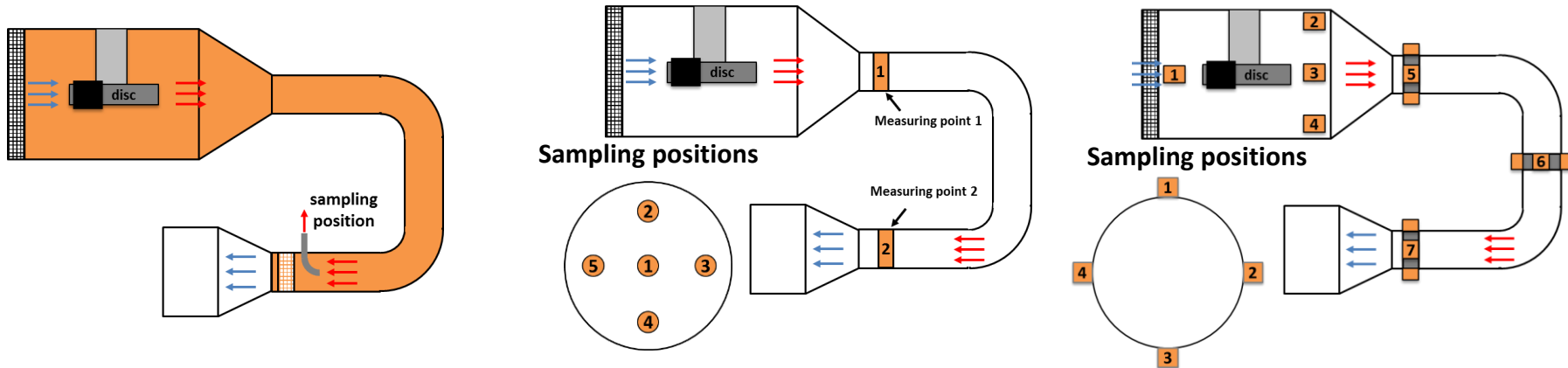
- according to preliminary examinations: the application of empirical models is not sufficient
- The application of complex software (mathematical-physical models)
 - high quality of results can be achieved
- validation methods for verifying the results of numerical flow simulation are necessary



3. Validation methods

Overview

1. Mass balance of deposited particles	2. Verification of the concentration profile	3. Verification of deposited particles
<ul style="list-style-type: none"> • filter based methodology • Verification of the transport efficiency of a sampling system • Analysis of the influence of different process parameters on the transport efficiency 	<ul style="list-style-type: none"> • verification of the size-resolved number concentration and uniformity • Analysis of the influence of different process parameters on the transport efficiency and uniformity 	<ul style="list-style-type: none"> • Analysis of size-resolved particle deposits and particle loss mechanism • Analysis of the uniformity of number concentration • Analysis of the influence of different process parameters • Analysis of the influence of material properties (electrostatics) or surface texture (roughness)



3. Validation methods

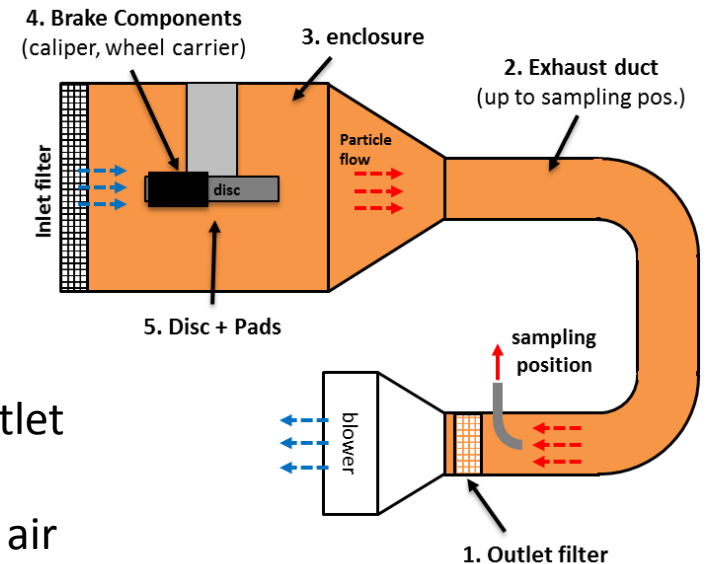
Method 1 – Filter-based determination of the particle mass balance

Verification of the transport efficiency of a sampling system (without size resolution)

- Weighing of deposited particle mass

Methodology:

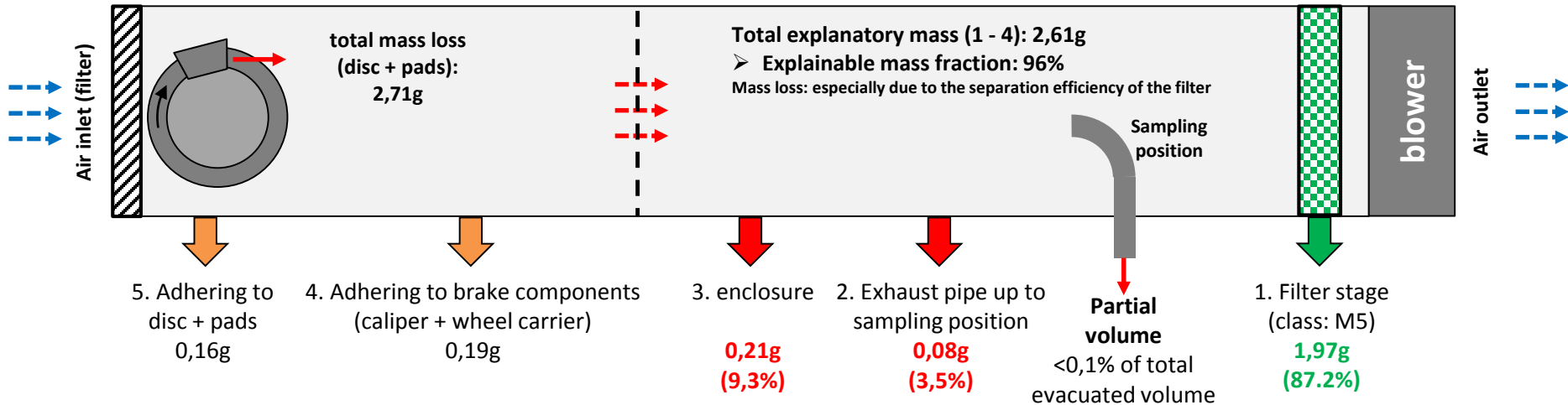
1. Integration of an outlet filter (fine dust - class M5) at the sampling position
2. Execution of the test-cycle as specified (blower activated - evacuation of emitted particles)
3. Determination of mass increase of the loaded outlet filter (Nr. 1)
4. Evacuation of deposited particles by compressed air (blower activated) and integrated filter (Nr. 2 – 5)
5. Weighing of mass increase of the filter stage per section as well as loss of disk and pads
6. Calculation of the mass-based transport efficiency
 - **Comparison of deposited particle mass vs. evacuated particle mass**



3. Validation methods

Method 1 – Filter-based determination of the particle mass balance

Test conditions: 60x 80 → 30km/h; 30bar; $T_{init} = 100^{\circ}\text{C}$



Calculation of the mass-based transport efficiency (without size resolution):

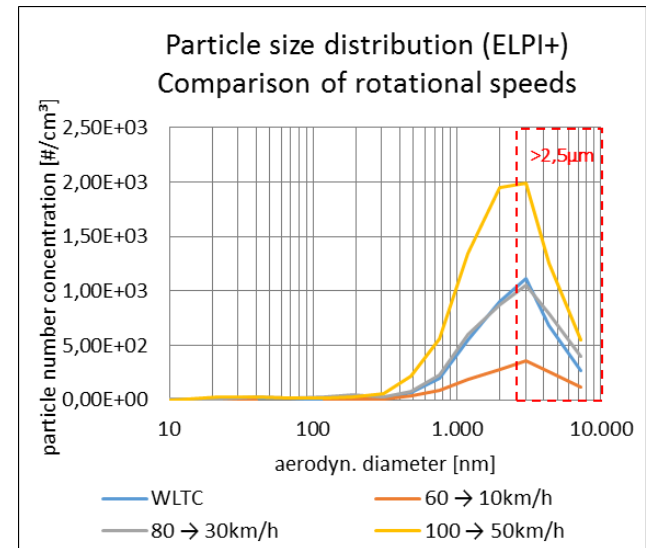
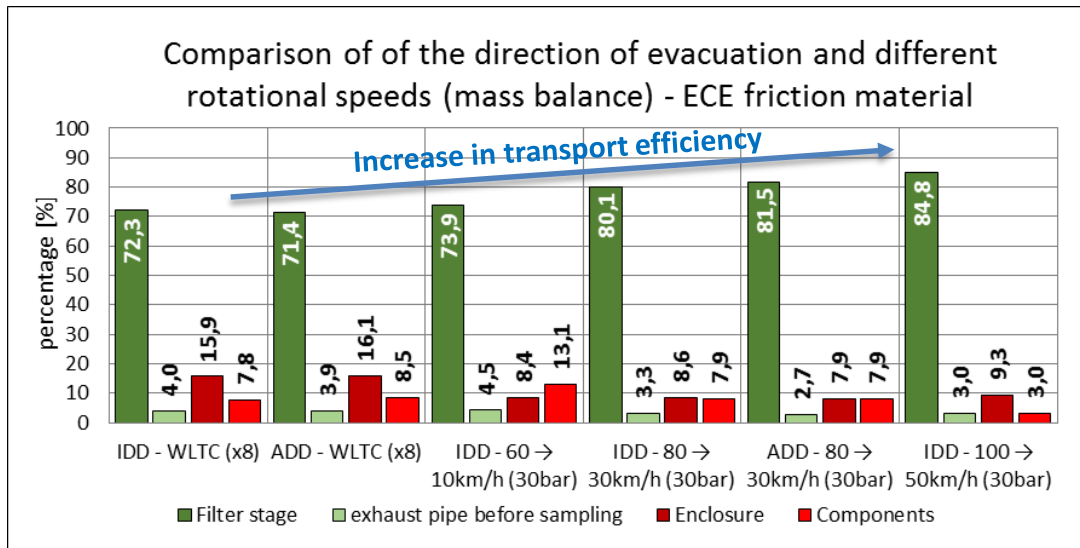
1. Detection of particle mass (deposited / evacuated) per section of the sampling system
2. Comparison of the sum of deposited mass (2 + 3) with the evacuated particle mass (1)

	Total (1-3)	Mass loss fraction (2+3)	Evacuated mass fraction (1)
Σ mass fraction	2,26g	0,29g ➤ Percentage: 12.8%	1,97g ➤ Percentage: 87.2% (transport efficiency)

3. Validation methods

Method 1 – Filter-based determination of the particle mass balance

Influence of the direction of evacuation and rotational speed

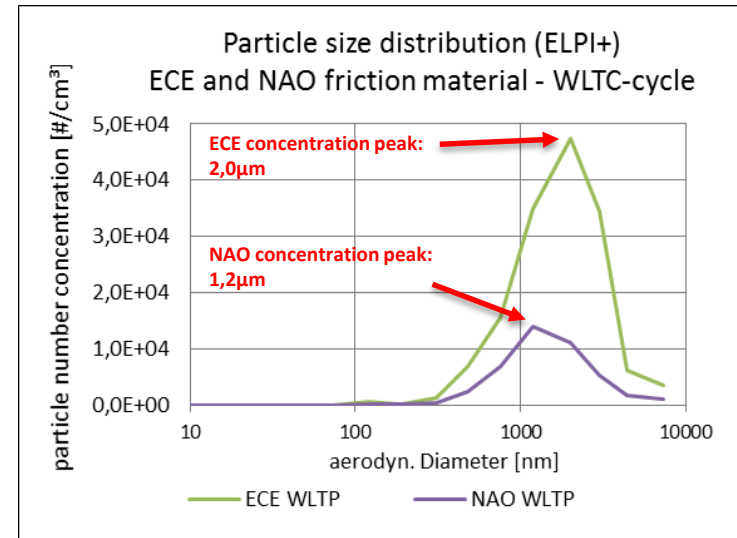
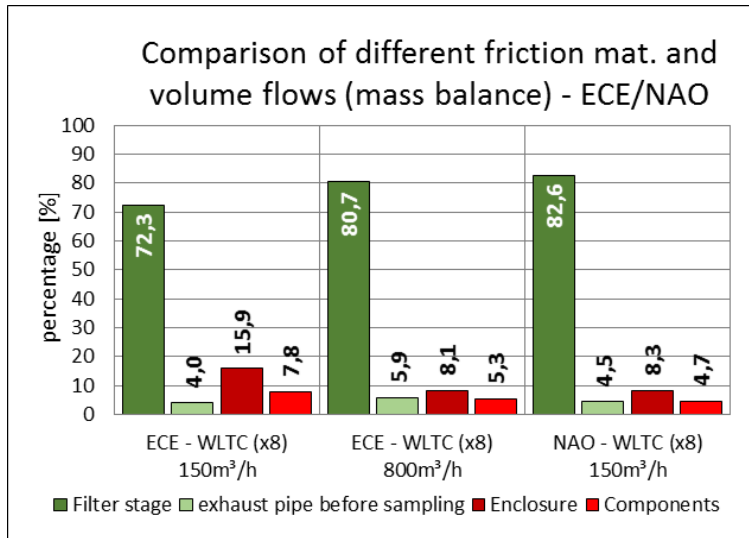


- **IDD: Evacuation in driving direction / ADD: Evacuation against driving direction**
- Mass-based transport efficiency depends on the rotational speed and friction energy
 - Change of the PSD with increase of the friction energy (red. of the CMD)
 - Increase in efficiency of evacuation for smaller particle diameter
- Deposition with variation of the suction direction depends on the initial speed
- Deposition at the components (e.g. caliper) depends on the rot. speed and the disc ventilation

3. Validation methods

Method 1 – Filter-based determination of the particle mass balance

Influence of different friction materials and volume flows

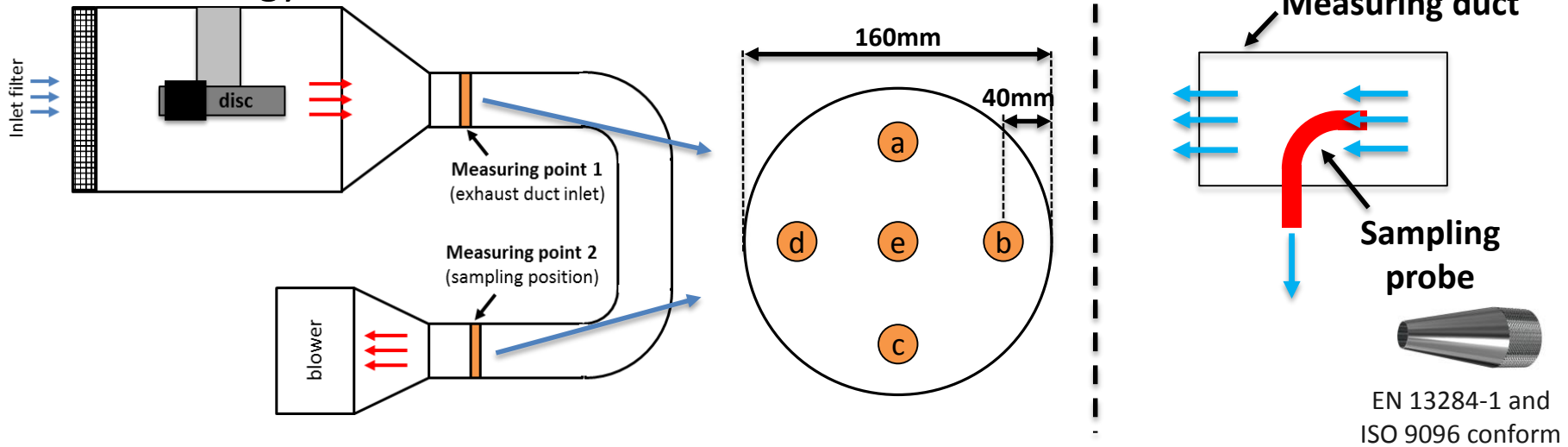


- NAO with a higher transport efficiency due to smaller particle diameter
- Increase transport efficiency with increasing volume flow
 - higher proportion of deposition in the exhaust duct (influence of transport loss mechanism: impaction / turbulent inertial deposition especially for particles larger than 1µm)

3. Validation methods

Method 2 – Verification of the concentration profile

Methodology



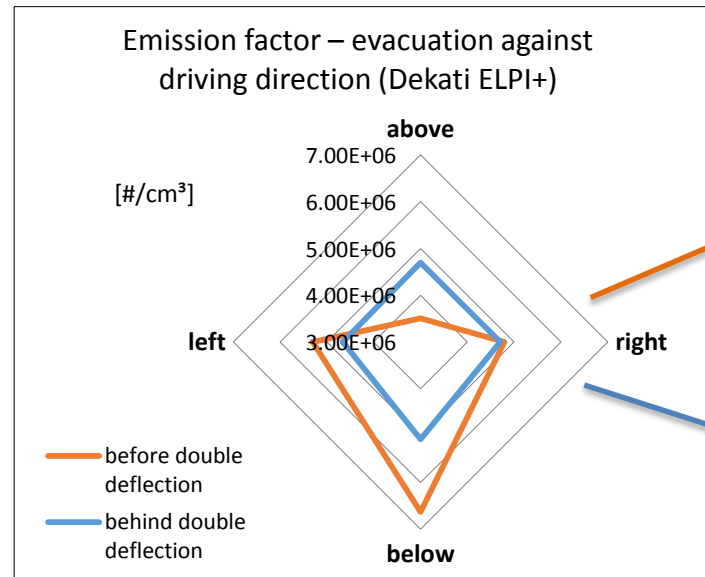
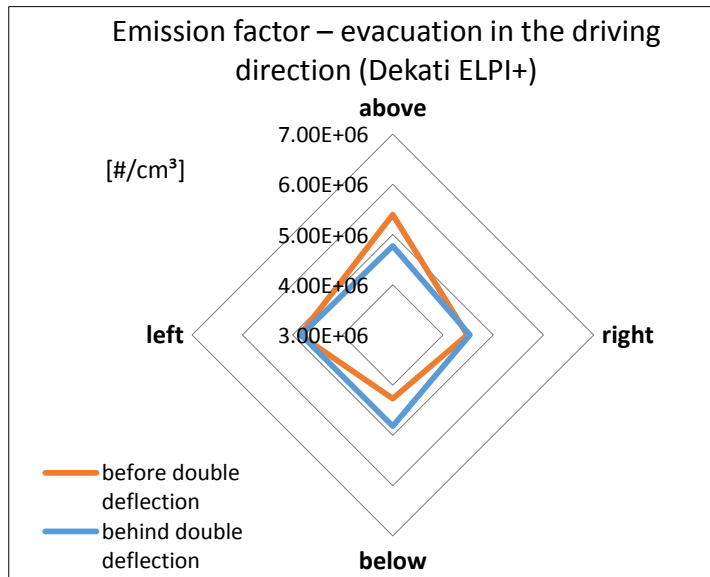
Methodology:

1. definition of the measuring target: Comparison of the concentration profile before and after the double deflection - sampling (isokinetic / isoaxial)
 - a. 4 positions offset by 90°
 - b. detection at the central point (e) serves as benchmark
2. Execution of the test-cycle as specified (blower activated) and measure the size resolved number concentration over the cross section (Dekati ELPI+: 6 – 10.000nm)

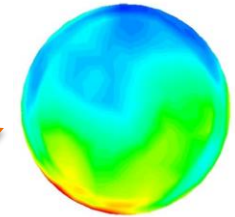
3. Validation methods

Method 2 – Verification of the concentration profile

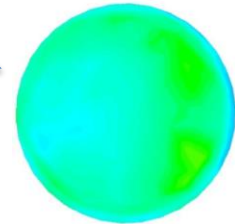
Comparison of the number of particles at different suction directions



before double deflection
uniformity: 80,9%



after double deflection
uniformity: 91,4%

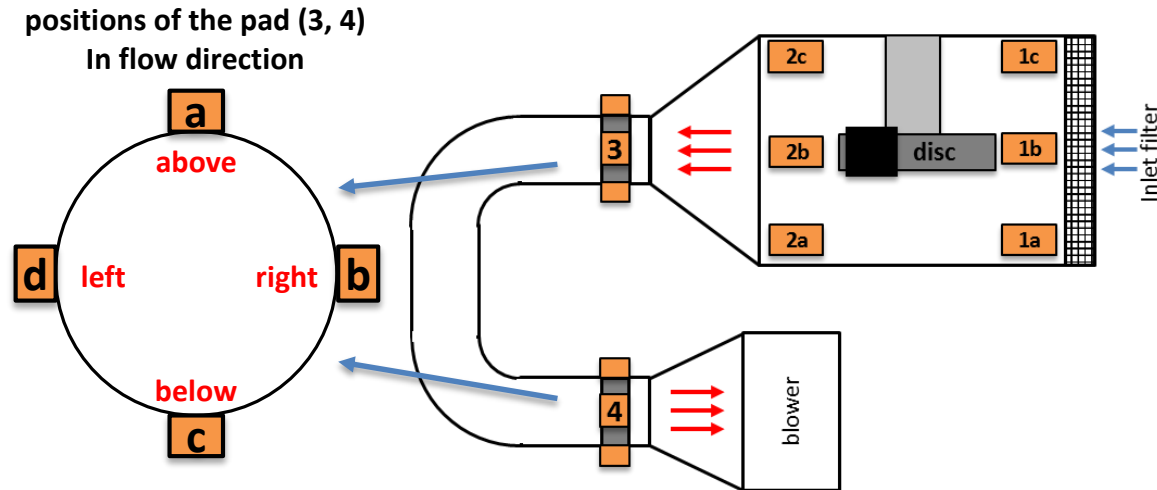


- test conditions: $v = 80 \rightarrow 30\text{km/h}$, $p = 30\text{bar}$, $T_{\text{init}} = 100^\circ\text{C}$; ECE – with copper
- The concentration profile is influenced by the evacuation direction
 - evacuation in driving direction: higher proportion above, lower proportion below
 - evacuation against driving direction: lower proportion above, higher proportion below
- significantly more homogeneous particle distribution due to double deflection

3. Validation methods

Method 3 – Verification of particle deposition mechanisms

Comparison of the size distribution at different suction directions



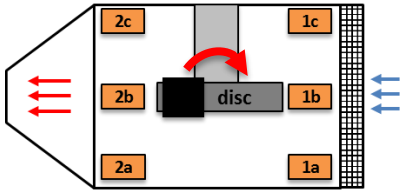
Methodology:

1. adaption of sampling pads in the duct (same material properties and surface texture)
 - positions: 2x4 pads offset by 90° (analysis of PSD and particle loss mechanism)
2. execution of the test-cycle as specified
3. removal of the collection plates and performing a microscopic analysis (1.000x)
4. analysis of microscopic images by software (e.g. scientific counter) - determination of the particle area and calculation of an equivalent diameter

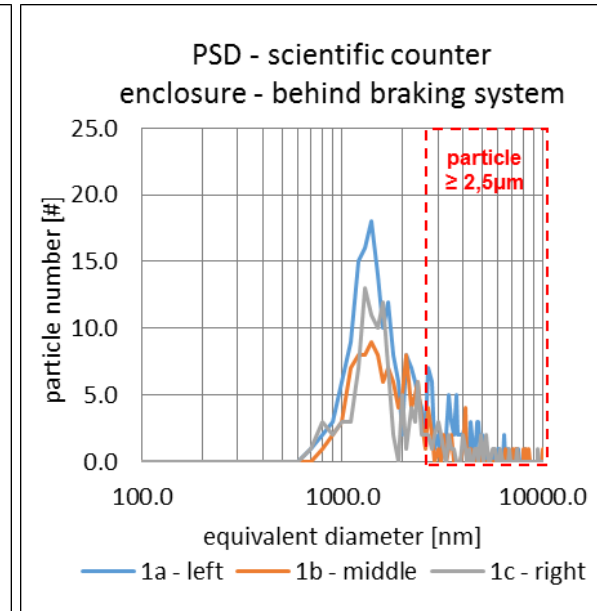
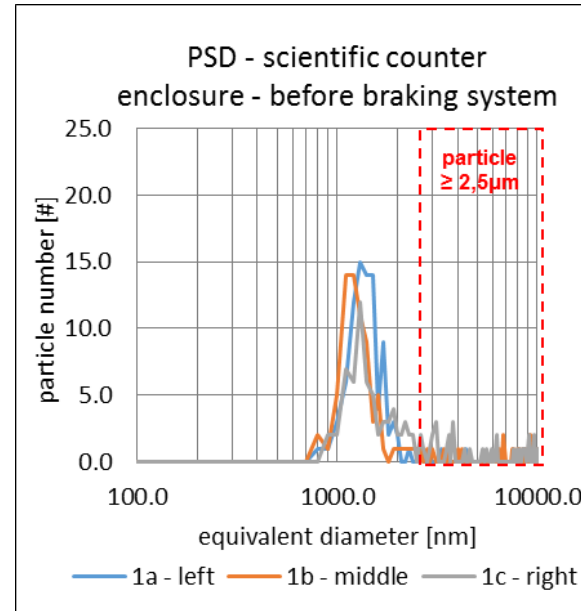
3. Validation methods

Method 3 – Verification of particle deposition mechanisms

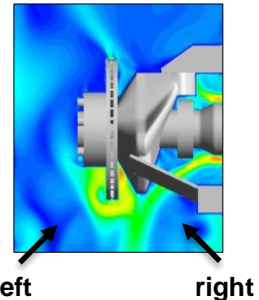
Comparison of the PSD of deposited particles (evacuation against driving direct.)



	before braking system (1)		behind braking system (2)	
	PM2.5 to PM10 [%]	CMD [μm]	PM2.5 to PM10 [%]	CMD [μm]
right (c)	65,0	1,74	79,5	1,87
middle (b)	76,1	1,28	80,5	1,92
left (a)	96,5	1,47	75,3	1,92



- Test conditions: $v = 60 \times 80 \rightarrow 30\text{km/h}$, $p = 30\text{bar}$, $T_{\text{init}} = 100^\circ\text{C}$; ECE-friction mat.
- Significant fraction of deposited particles smaller than $1\mu\text{m}$
- High proportion (35,0%) of deposited particles $>2.5\mu\text{m}$ on the right before the braking system, low percentage on the left (3,5%)
 - influence of “dead water areas” due to the adapted wheel carrier

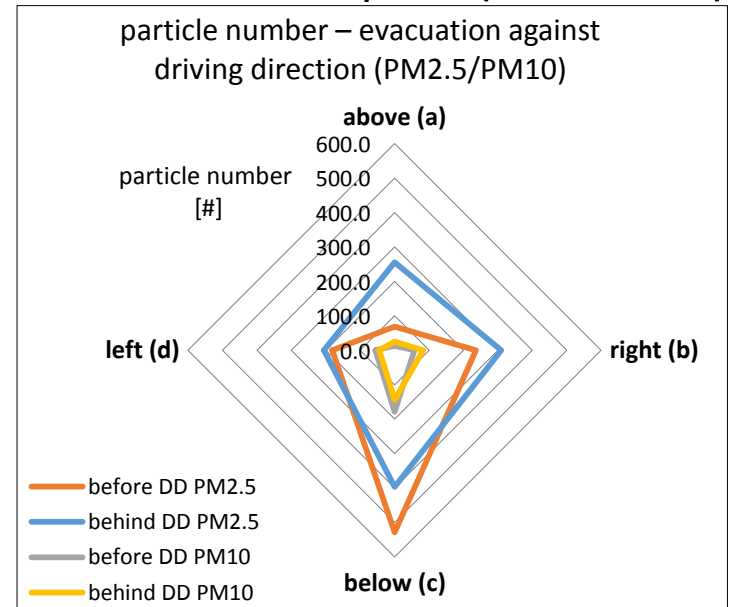
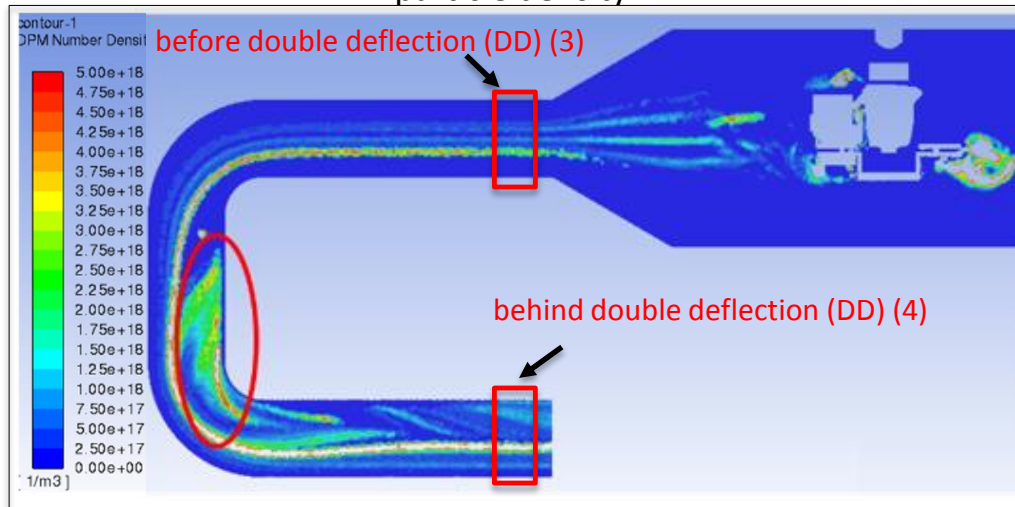


3. Validation methods

Method 3 – Verification of particle deposition mechanisms

Comparison of the PSD of deposited particles – on collection pads (evac. ADD)

flow simulation – RSM stress omega
particle density

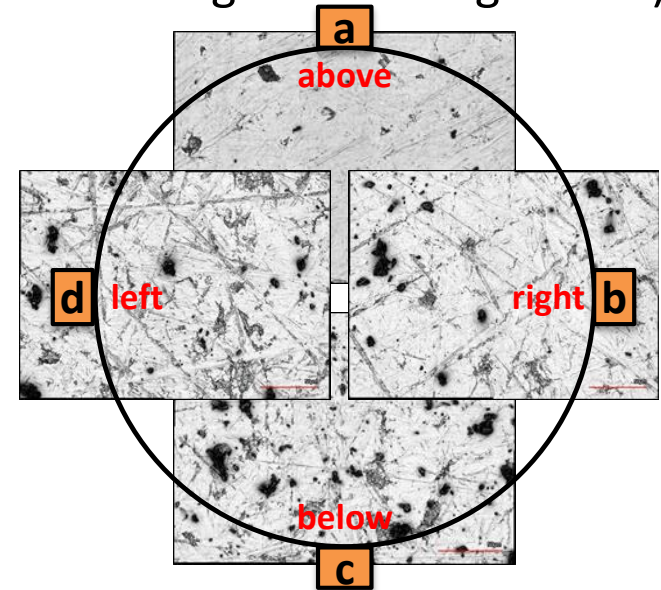
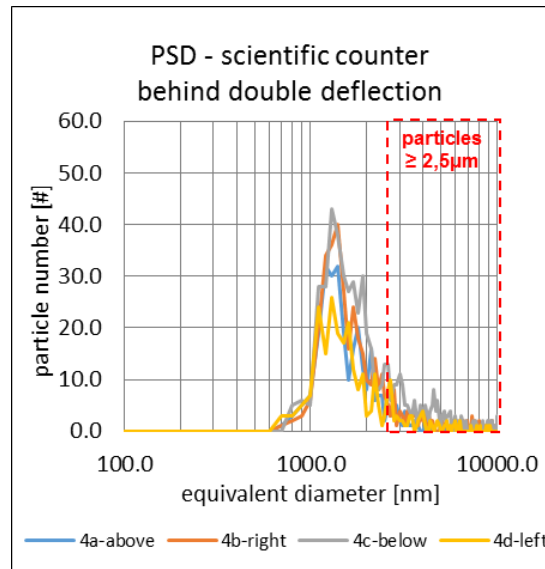
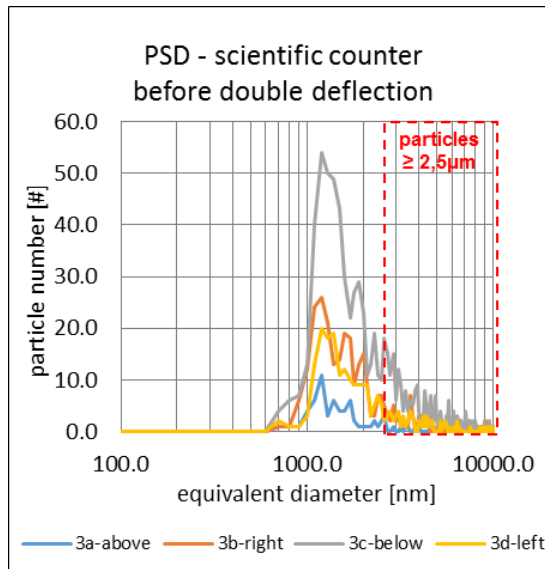


- The expression of a vortex after the first curvature causes an increase in uniformity
- Increase in the homogenization of the flow profile (uniformity) with simultaneous shift of the concentration profile after the double deflection to the right
 - Comparison of flow simulation and validation: **High degree of agreement at current state of flow study**

3. Validation methods

Method 3 – Verification of particle deposition mechanisms

Comparison of the PSD of deposited particles (evacuation against driving direct.)



- Influence of the double deflection is also evident with regard to deposited particles in a homogenization of the flow profile
- Highest proportion of deposited particles $>2,5\mu\text{m}$ in the lower area (25,2%/26,6%), lowest in the upper area (15,9%/8,9%)
 - Proportion is increased with increasing length of the exhaust duct by external processes (e.g. sedimentation, turbulent inertial deposition)

	before double deflection (3)		behind double deflection (4)	
	#-PM2.5 to #-PM10 [%]	CMD [μm]	#-PM2.5 to #-PM10 [%]	CMD [μm]
above (a)	84,1	1,44	91,1	1,40
right (b)	80,3	1,69	78,9	1,62
below (c)	74,8	1,82	73,4	2,01
left (d)	76,4	1,84	82,0	1,63

4. Conclusions

- Application, improvement and validation of CFD models is necessary for the development of a CVS
- By use of the methods presented, the transport efficiency and uniformity of number concentration of different sampling systems (mobile or stationary) can be verified – CFD results can be validated
- The transport efficiency of a sampling systems (CVS) depends from various influence factors (tribological and sampling conditions)
- Geometric adjustments can increase uniformity (double deflection)
 - **Evaluated and validated methodology for the development of sampling systems is available**

5. Outlook

- Application of the presented methods for the verification of particle deposition / adhesion mechanisms on the transport efficiency and uniformity of the number concentration
 - stationary and mobile sampling systems
- findings regarding brake dust particle deposition mechanisms and particle properties can be used to improve CFD models
- by using advanced models the CVS design can be enhanced

Thank you for your attention!



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