



**GTR#13 meeting**

**5-7 February 2019, Vancouver**

# **GTR#13 engulfing and localised tests: further analysis**

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# Definitions

**Heat release rate (HRR)**

- Heat release rate in a fire [kW] (can easily be measured by propane flow rate to a burner).

**Specific heat release rate (HRR/A)**

- Heat release rate in a fire, HRR, divided by the area of fire source, A, [kW/m<sup>2</sup>]

**Heat flux,  $\dot{q}''$**

- Heat flux on tank surface [kW/m<sup>2</sup>] (**not the same as HRR/A even dimension is the same!**).

**Fire resistance rating (FRR, **required by first responders – EU HyResponse project**)**

- Time from burner ignition until container rupture in a fire (without TPRD or failed TPRD or localised fire far from TPRD)



# Part 1. Engulfing fire

# GTR#13 temperature requirements

## 6.2.5.2. Engulfing fire test

### GTR#13 fire test requirements:

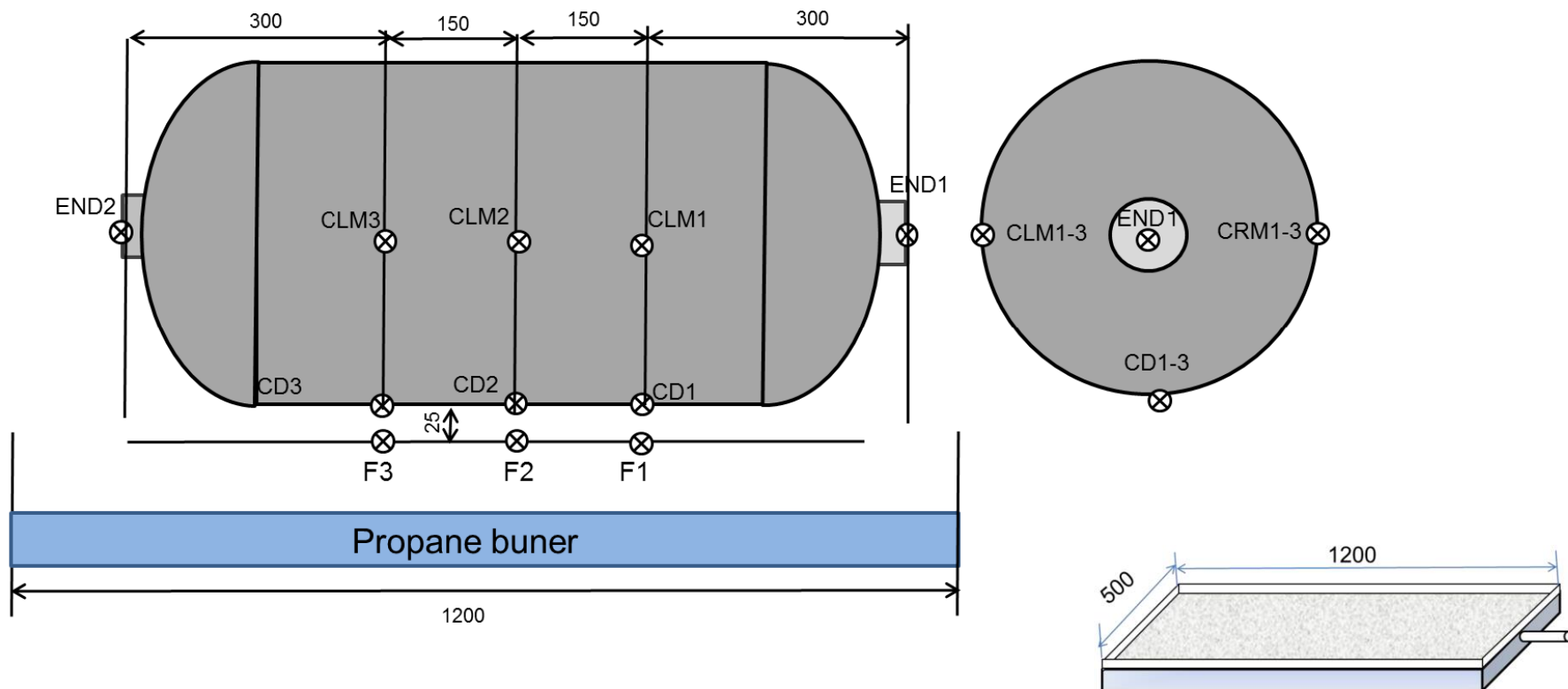
“Within five minutes after the fire is ignited, an average flame temperature of **not less than 590°C** (as determined by the average of the two thermocouples recording the highest temperatures over a 60 second interval) **is attained and maintained for the duration of the test.**”

# JARI test with blanket burner

## Description

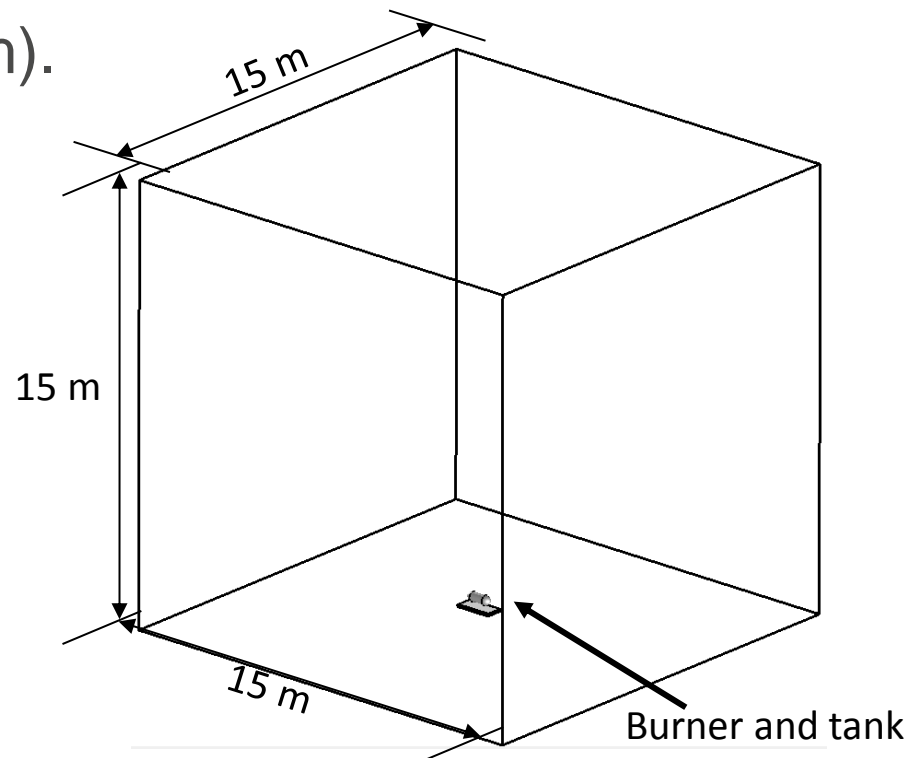
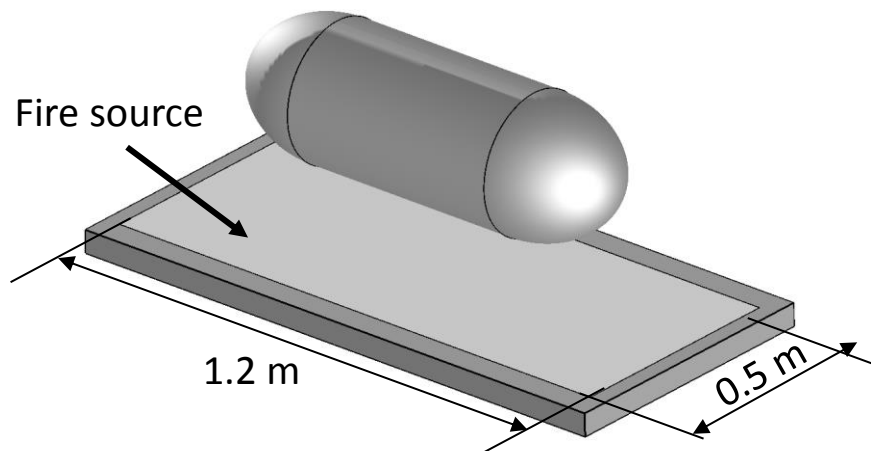
Propane ( $C_3H_8$ ) flow rate  $\dot{V}=100$  NL/min ( $\dot{m}=3$  g/s),  
blanket burner of area  $A=0.6$  m<sup>2</sup> with HRR=0.137 MW.

Thus, specific heat release rate is **HRR/A=0.228 MW/m<sup>2</sup>**.



# Ulster model (blanket burner test)

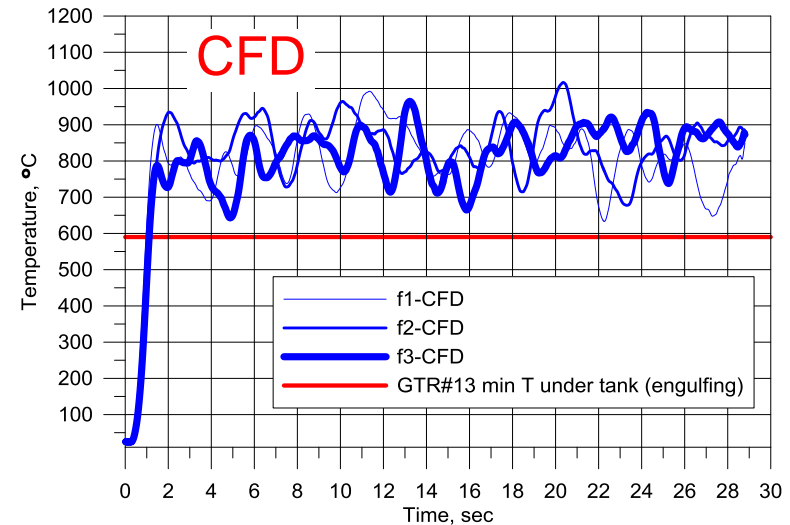
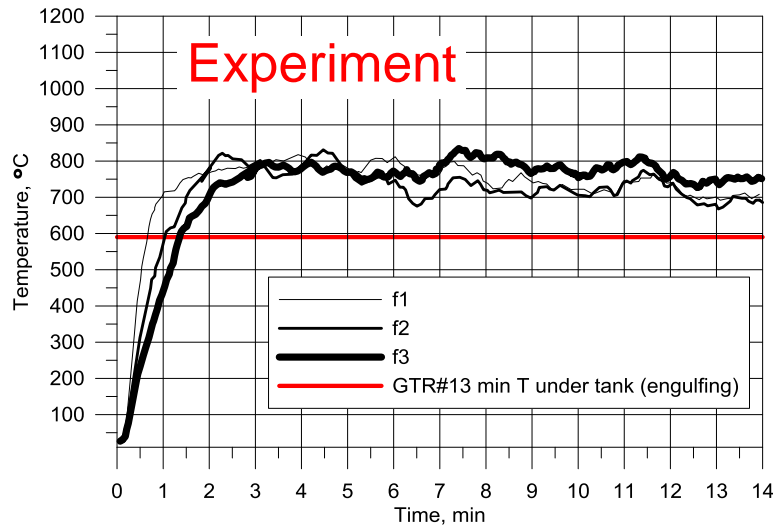
- Similar to JARI test the area of “blanket burner” is  $A=0.6 \text{ m}^2$  ( $L \times W=1.2 \times 0.5 \text{ m}$ ). Velocity release: 3 mm/s.
- Burner is positioned 0.5 m above the ground.
- Large calculation domain:  $15 \times 15 \times 15 \text{ m}$ .
- Conjugate heat transfer from the fire to the Type 3 tank ( $L \times D=0.9 \times 0.3 \text{ m}$ ).



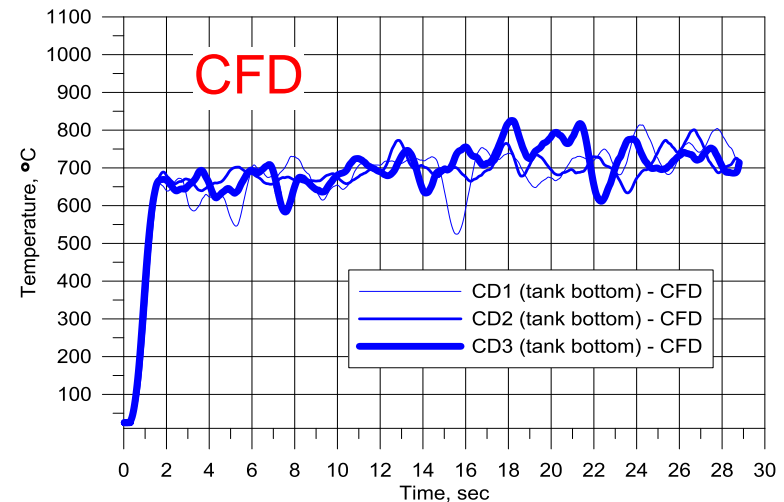
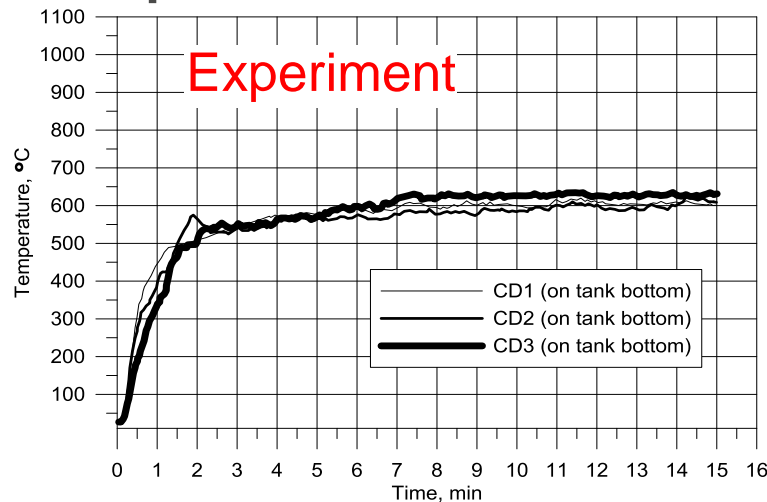
# Blanket burner: $HRR/A=0.228 \text{ MW/m}^2$

## CFD model validation (1/2)

Temperature: 25 mm under tank bottom (GTR#13 compliant)



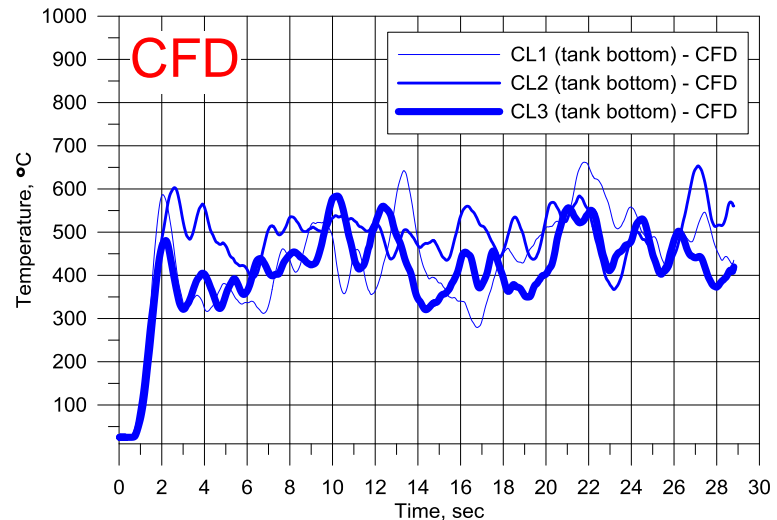
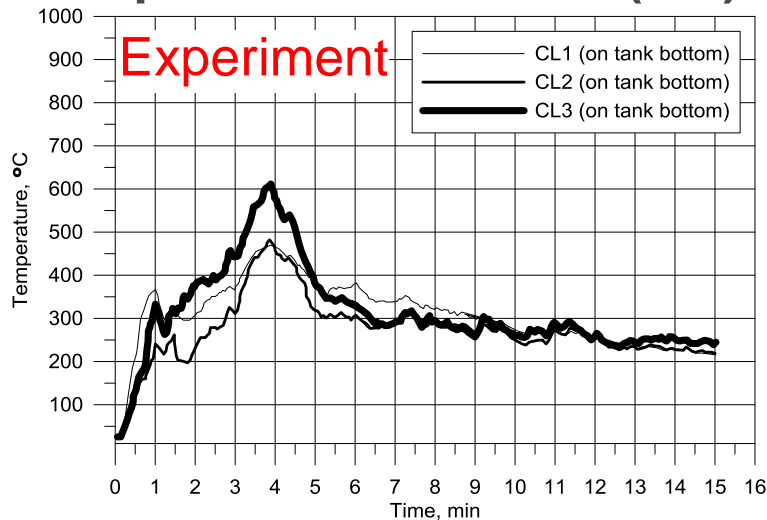
Temperature: tank bottom



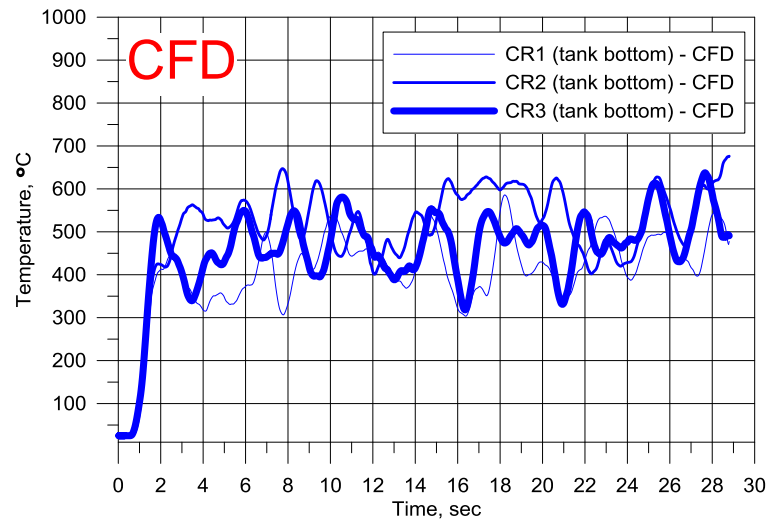
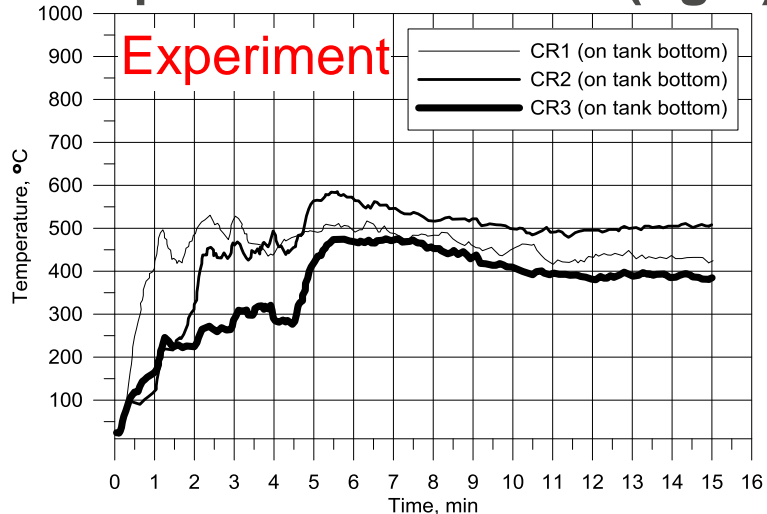
# Blanket burner: $HRR/A=0.228 \text{ MW/m}^2$

## CFD model validation (2/2)

### Temperature: tank side (left)



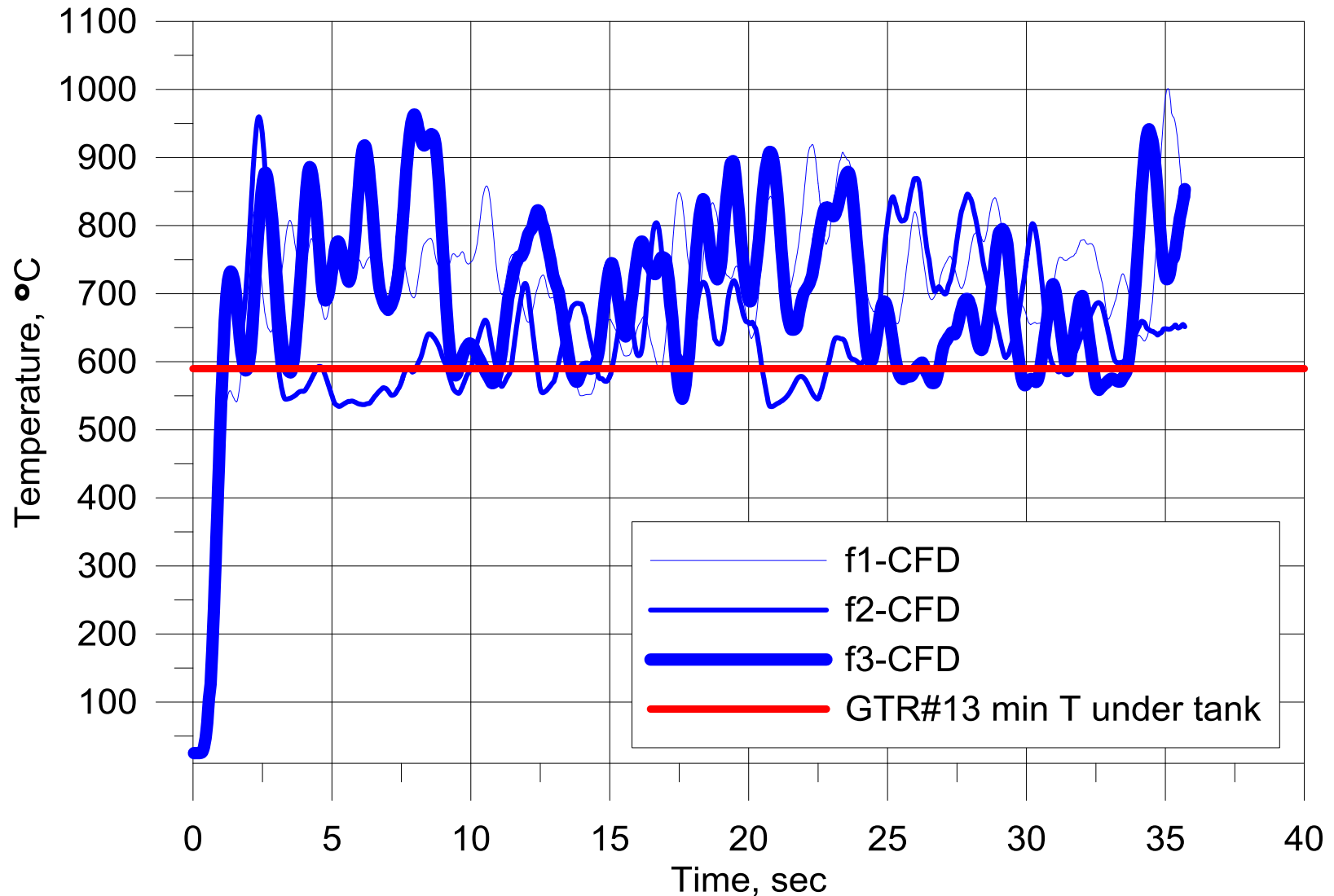
### Temperature: tank side (right)





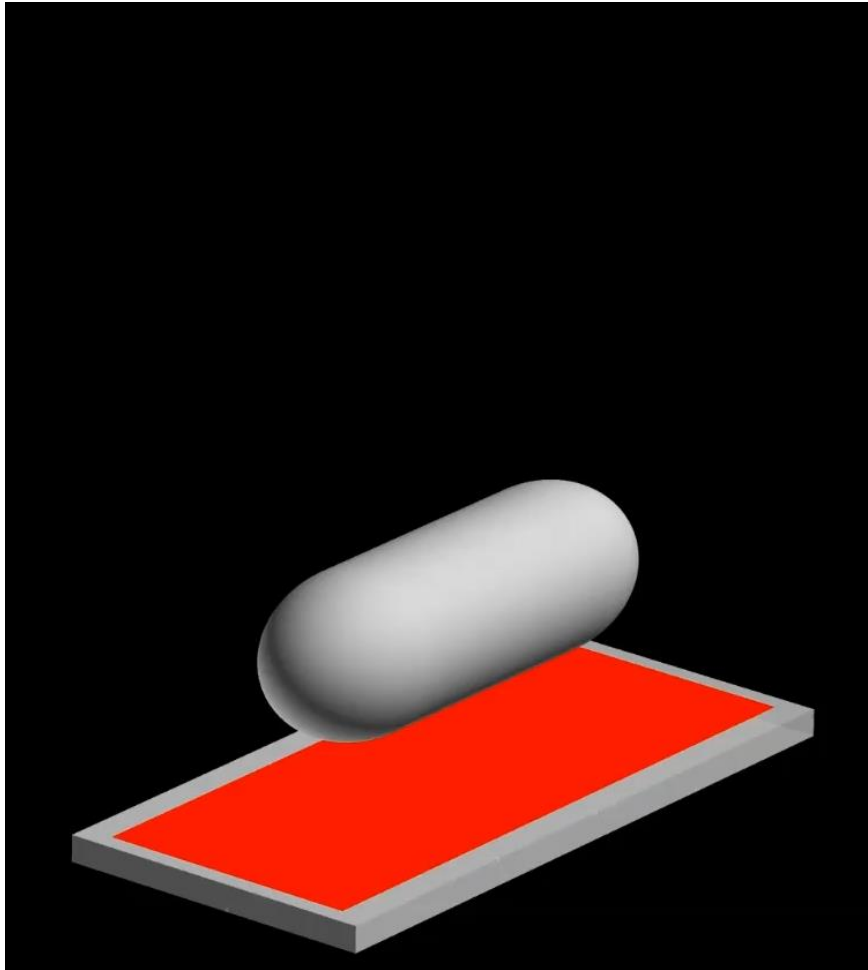
# Blanket burner: $HRR/A=1 \text{ MW/m}^2$

Temperature under tank (GTR#13 compliant!)

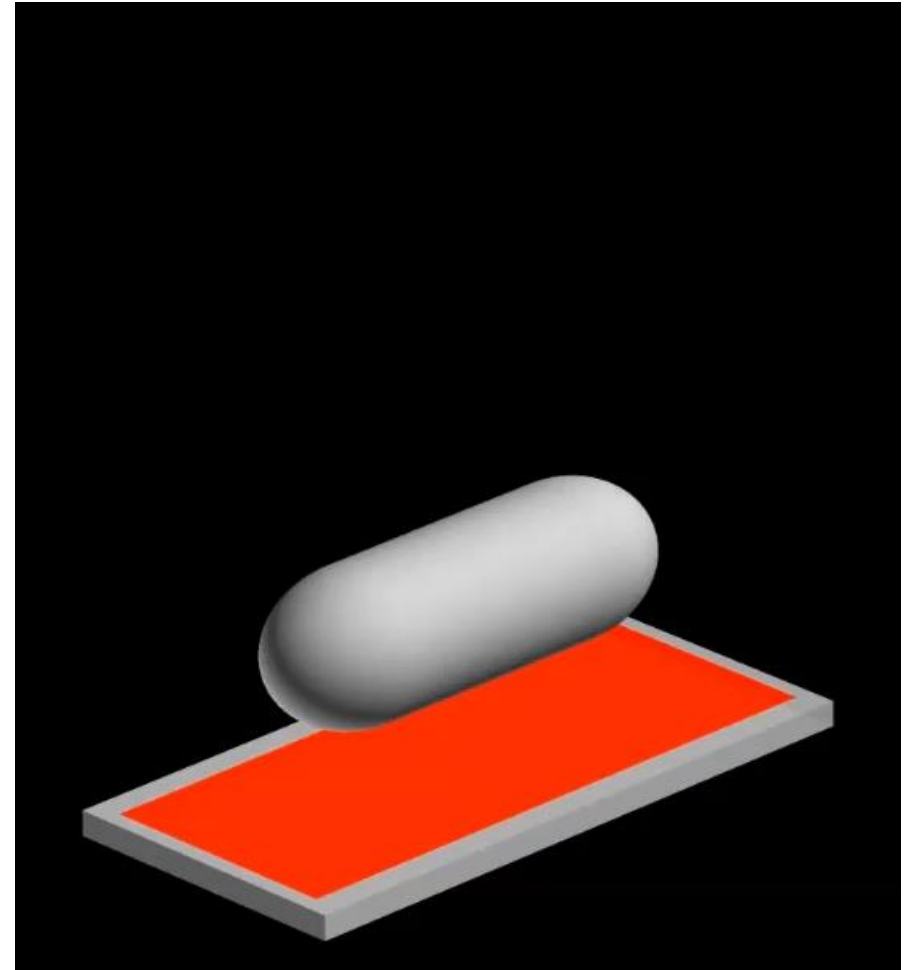


# Blanket burner: two different HRR/A

HRR/A=0.228 MW/m<sup>2</sup>



HRR/A=1 MW/m<sup>2</sup>

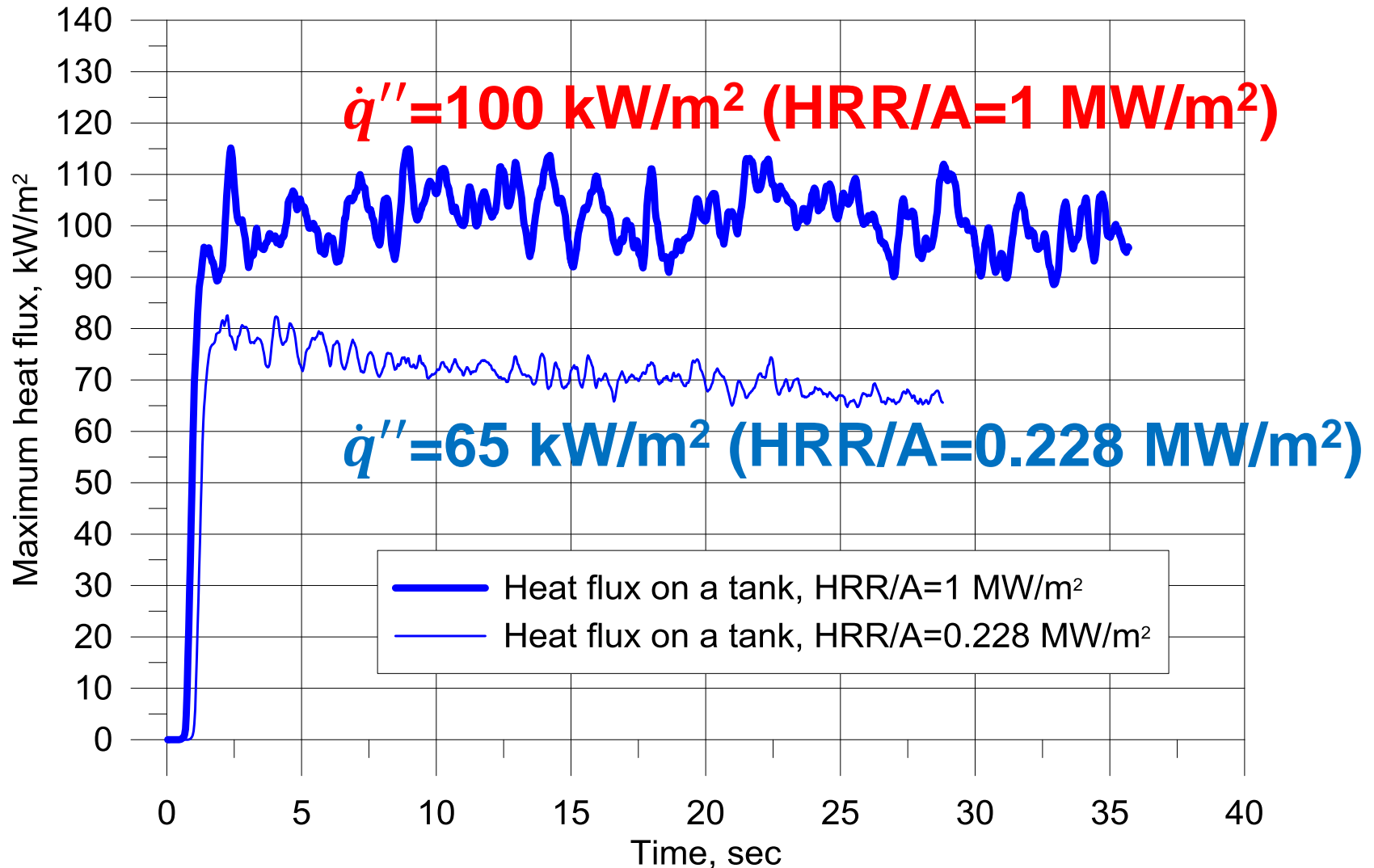


 590°C (GTR#13 min required)  1030°C  1230 °C

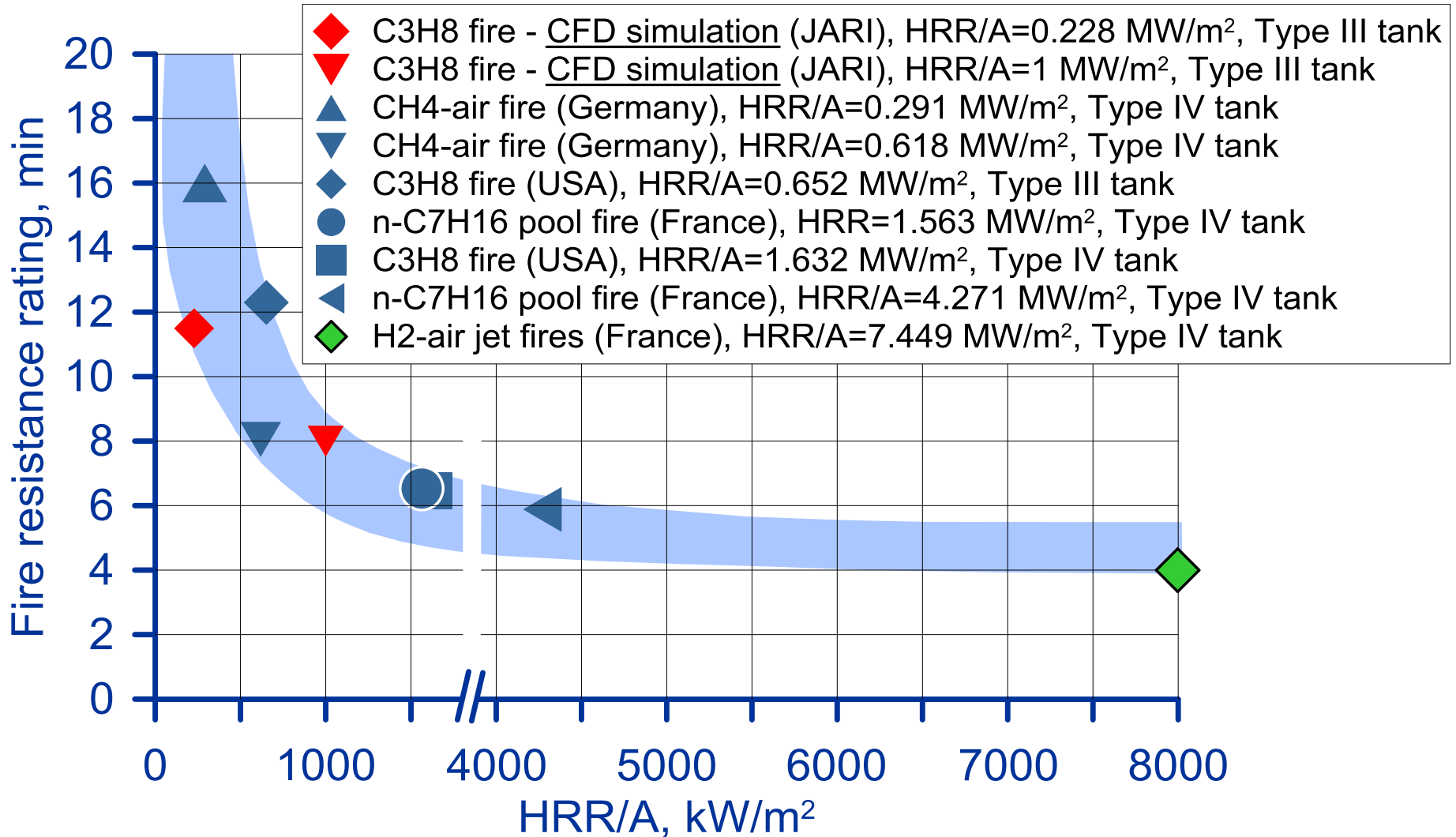
# Blanket burner: $\dot{q}''$ depends on HRR/A

## Reason of poor fire test reproducibility

GTR#13 temperature is satisfied but heat flux to tank ( $\dot{q}''$ ) is different



# FRR dependence on HRR/A

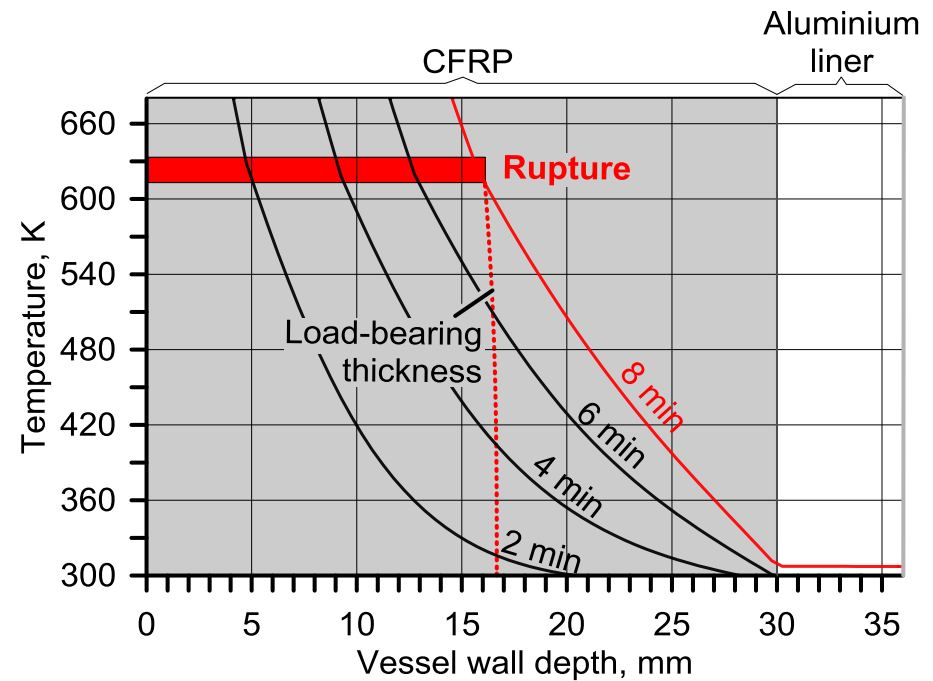
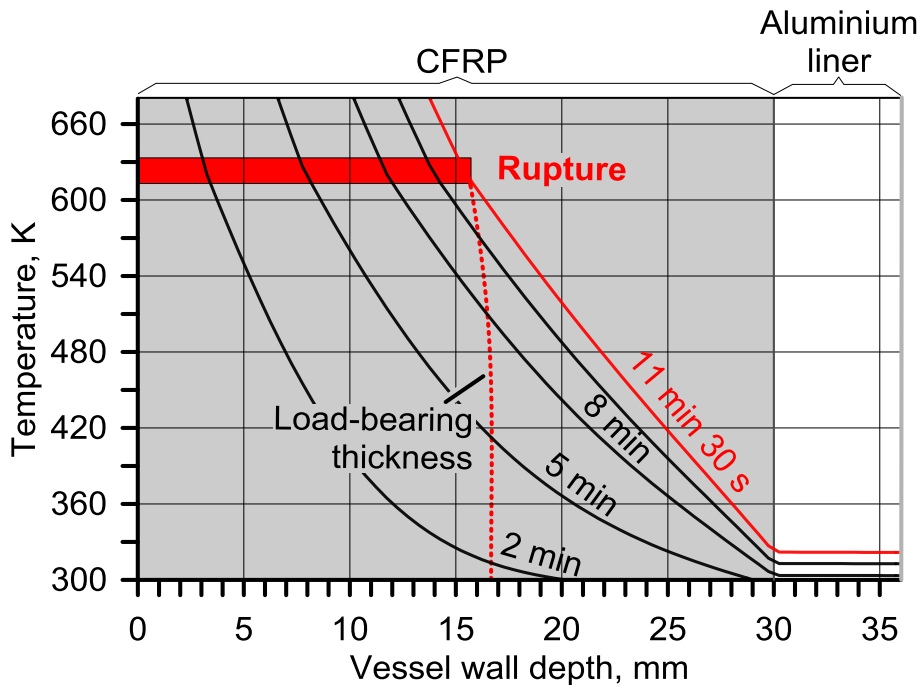


# Blanket burner: HRR/A defines FRR

## 700 bar Type 3 tank (0.9x0.3 m)

HRR/A=0.228 MW/m<sup>2</sup>

HRR/A=1 MW/m<sup>2</sup>



**Difference in FRR is 44%:**

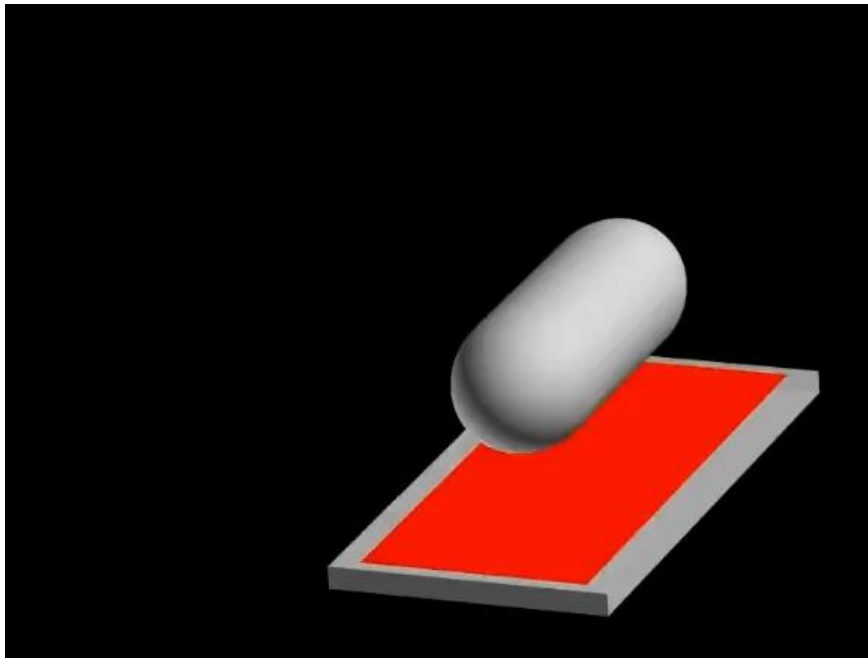
For HRR/A=0.228 MW/m<sup>2</sup> the FRR=11 min 30 s.

For HRR/A=1 MW/m<sup>2</sup> the FRR=8 min.

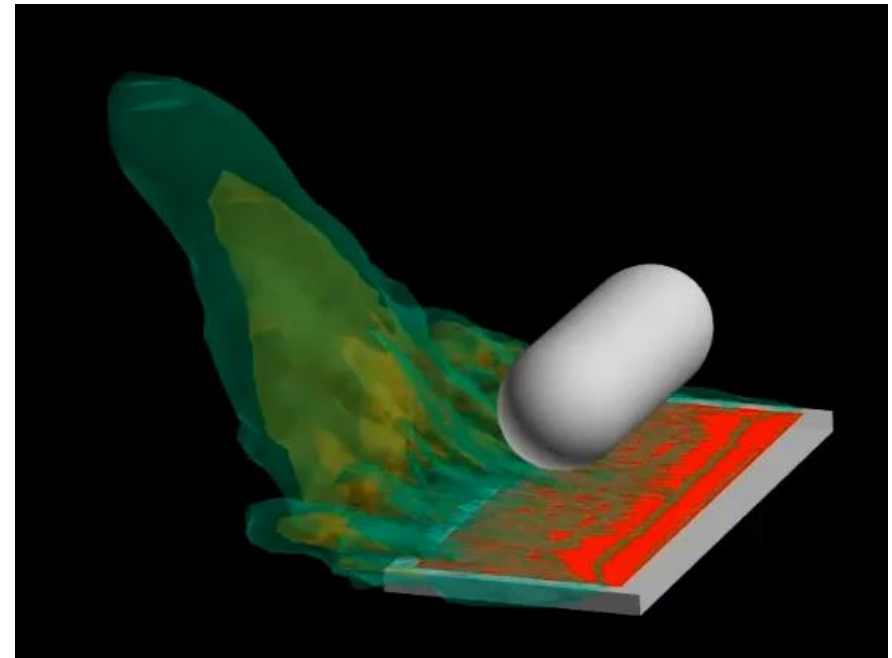
# Blanket burner: wind effect (1.8 m/s)

## Simulation video (temperature)

HRR/A=0.228 MW/m<sup>2</sup>



HRR/A=1 MW/m<sup>2</sup>



Temperatures:



590°C (GTR#13 min required)



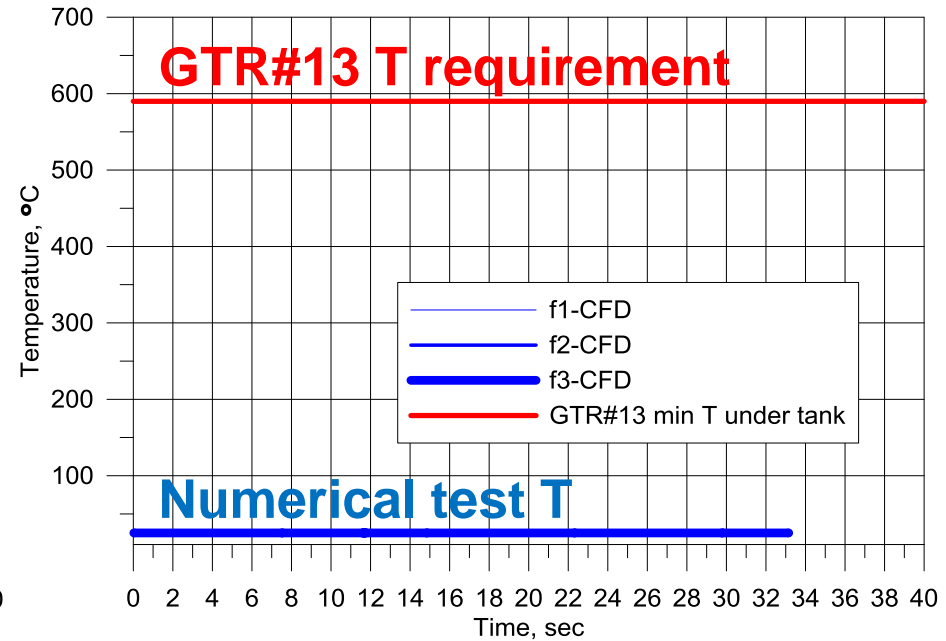
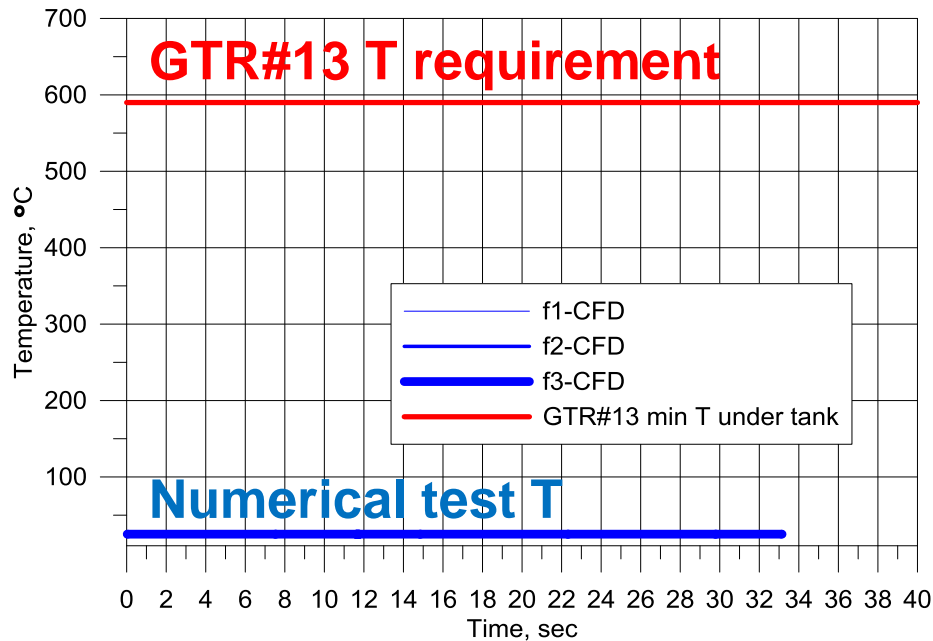
1030°C

# Blanket burner: wind effect (1.8 m/s)

## Temperature under tank (GTR#13 non-compliant)

HRR/A=0.228 MW/m<sup>2</sup>

HRR/A=1 MW/m<sup>2</sup>



In wind conditions (<1.8> m/s, Buxton, UK) GTR#13 minimum temperature requirements **are not satisfied: temperatures under the tank are close to ambient 20°C!**

# Intermediate remarks

## Blanket burner

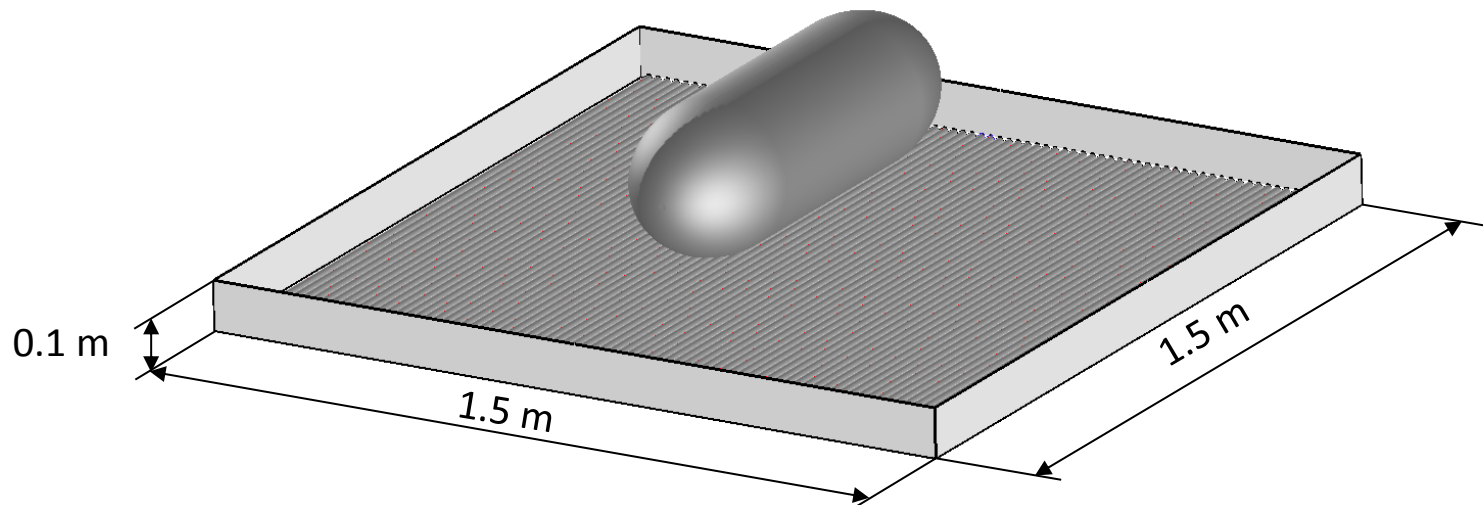
- Heat flux to a tank in fire with blanket burner increases by about 50% (from  $\dot{q}''=65$  kW/m<sup>2</sup> to  $\dot{q}''=100$  kW/m<sup>2</sup>) for the increase of HRR/A from 0.228 MW/m<sup>2</sup> to 1 MW/m<sup>2</sup>. This resulted in FRR decrease by 44% from 11.5 min to 8 min (GTR#13 temperature requirements are reproduced in both cases!).
- For no wind conditions, the fire test reproducibility can be provided for HRR/A > 1 MW/m<sup>2</sup> (as per “saturation graph”).
- Blanket burner of investigated size 500x1200 mm performance in a wind of order 1.8 m/s is a concern. Only “no wind” facilities could use it to satisfy GTR#13 temperature requirements.
- A new “wind-resistant” blanket burner is needed (increased size?).



# Pipe burner (1/2)

## Two HRR/A cases (same as JARI burner)

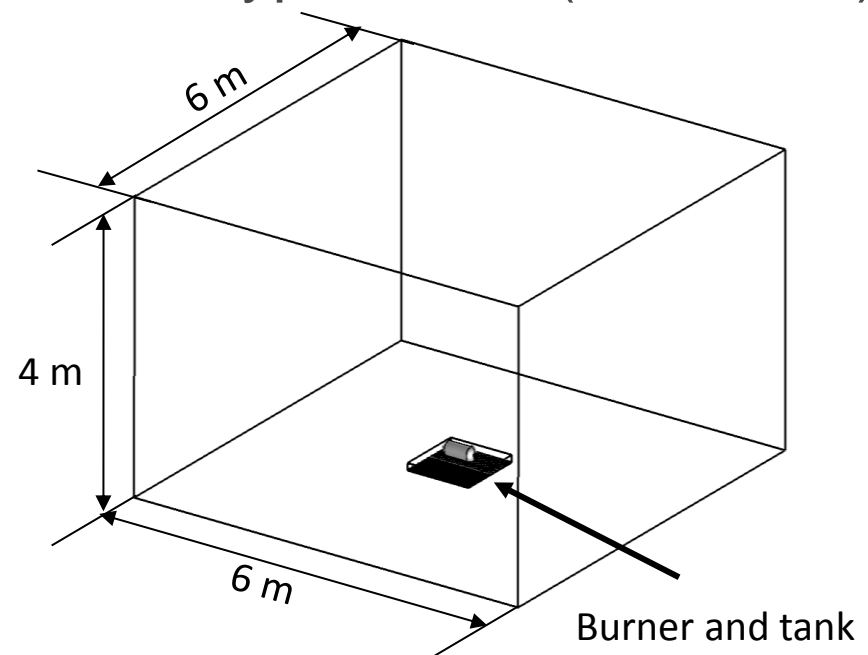
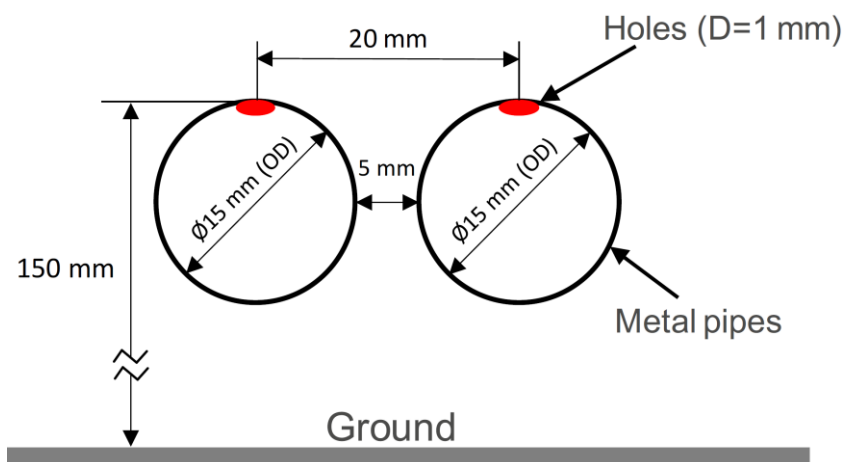
- **Case 1:** Propane ( $C_3H_8$ ) flow rate  $\dot{V}=362.4$  NL/min,  $\dot{m}=11.07$  g/s. Pipe burner area  $2.25$  m<sup>2</sup>, HRR= $0.513$  MW. Thus **HRR/A=0.228 MW/m<sup>2</sup>**.
- **Case 2:** Propane ( $C_3H_8$ ) flow rate  $\dot{V}=1589$  NL/min,  $\dot{m}=48.54$  g/s, HRR= $2.25$  MW. Thus **HRR/A=1 MW/m<sup>2</sup>**.
- With and without wind (1.8 m/s) study.



# Pipe burner (2/2)

## Numerical details

- 5600 holes spaced uniformly at 20 mm. Hole  $D=1$  mm.
- Propane velocity: 1.2 m/s ( $HRR/A=0.228$  MW/m<sup>2</sup>) and 5.3 m/s ( $HRR/A=1$  MW/m<sup>2</sup>). Note: 3 mm/s in blanket burner.
- Burner positioned at 0.15 m above the ground.
- Calculation domain: 6x6x4 m.
- Conjugate heat transfer from fire to Type 3 tank (0.9x0.3 m).

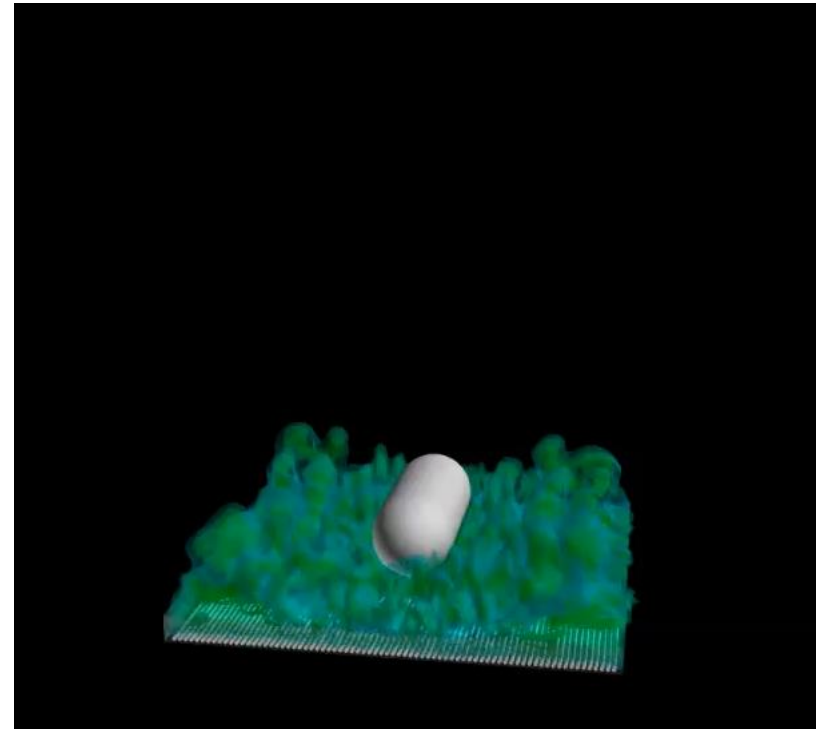
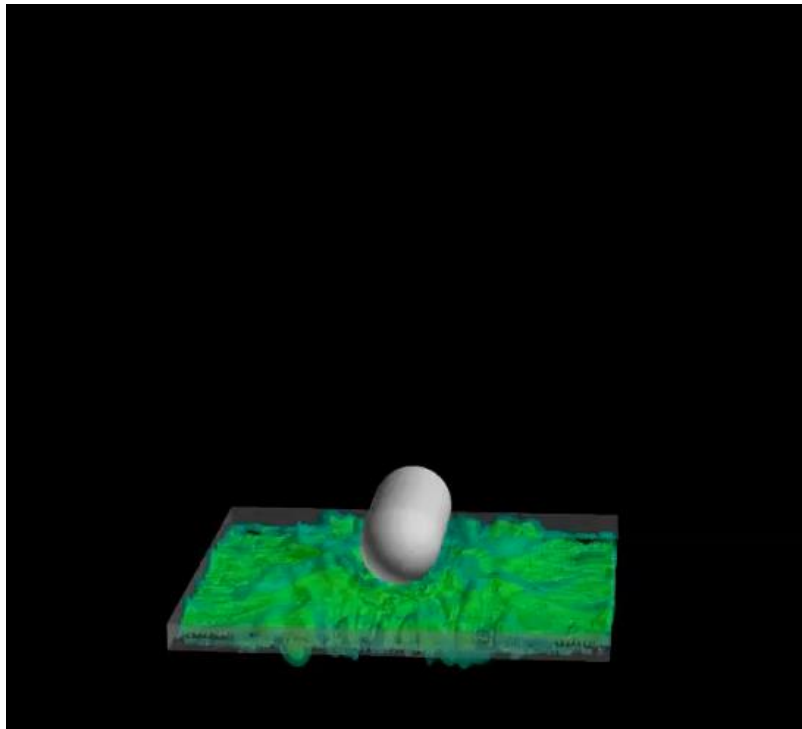


# Pipe burner: no wind

## Simulation video (temperature)

Case1:  $HRR/A=0.228 \text{ MW/m}^2$

Case 2:  $HRR/A=1 \text{ MW/m}^2$



Temperatures:



590°C (GTR#13 min required)



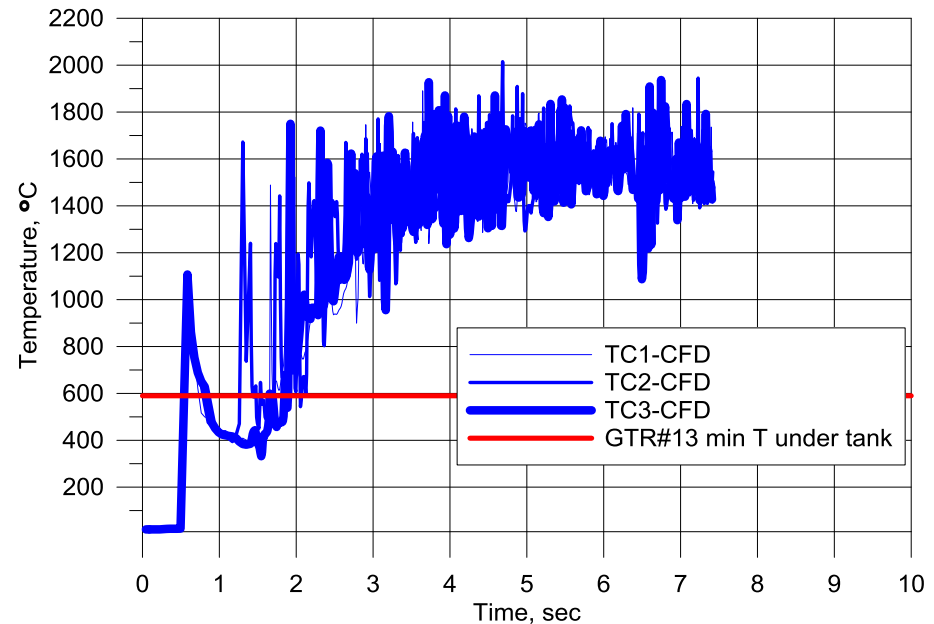
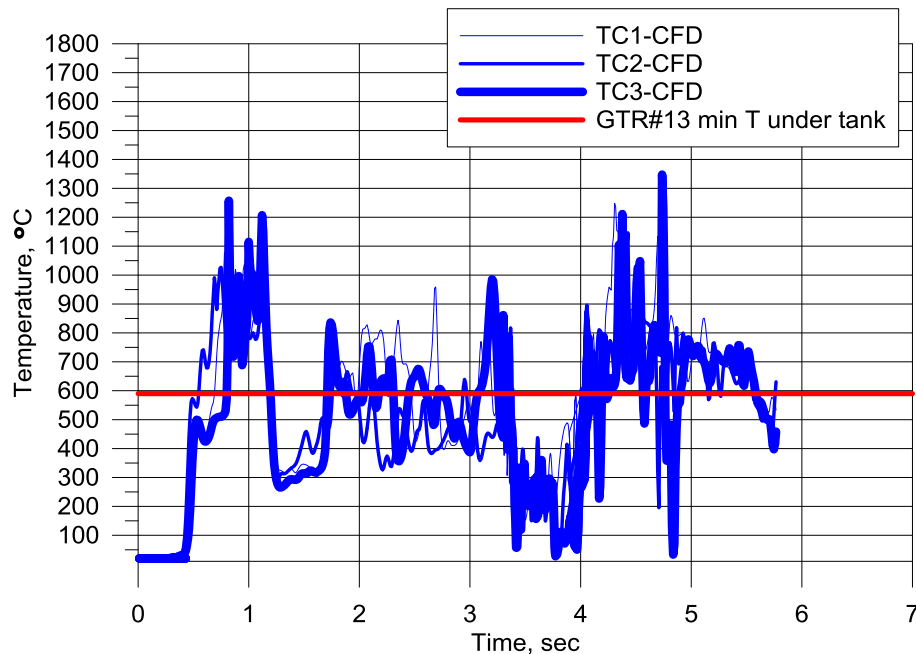
1030°C

# Pipe burner: no wind

## Temperature under tank (simulation)

Case1:  $HRR/A=0.228 \text{ MW/m}^2$

Case 2:  $HRR/A=1 \text{ MW/m}^2$

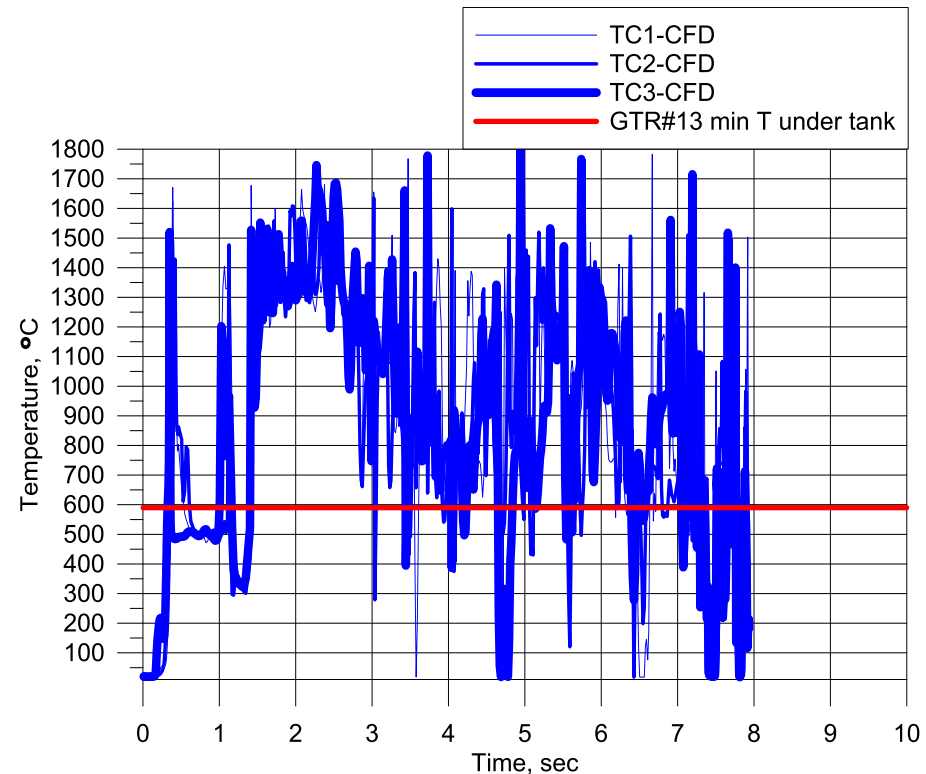
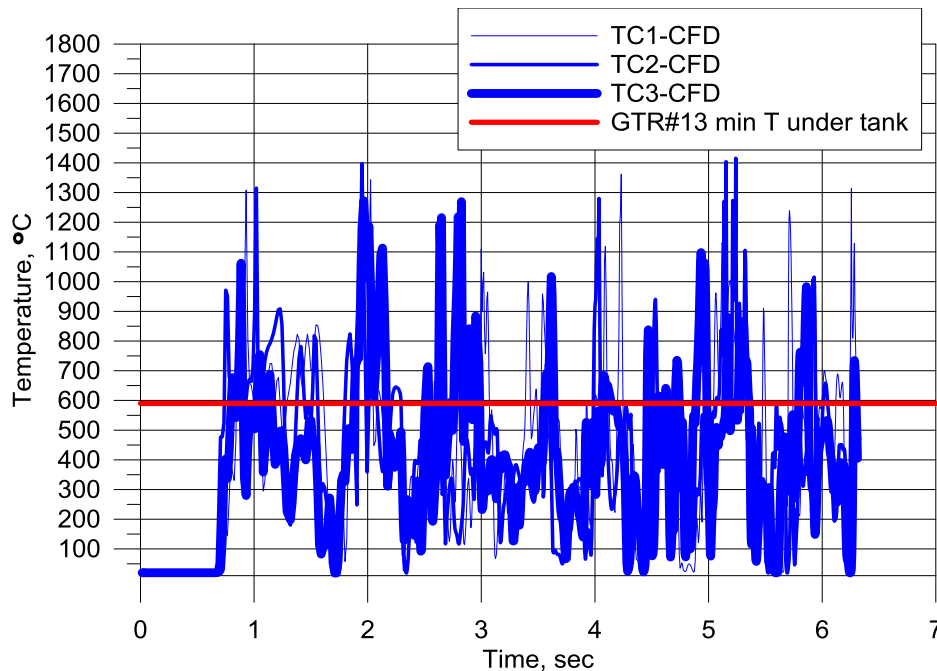


# Pipe burner: wind effect (1.8 m/s)

## Temperature under tank (simulation)

Case1:  $HRR/A=0.228 \text{ MW/m}^2$

Case 2:  $HRR/A=1 \text{ MW/m}^2$

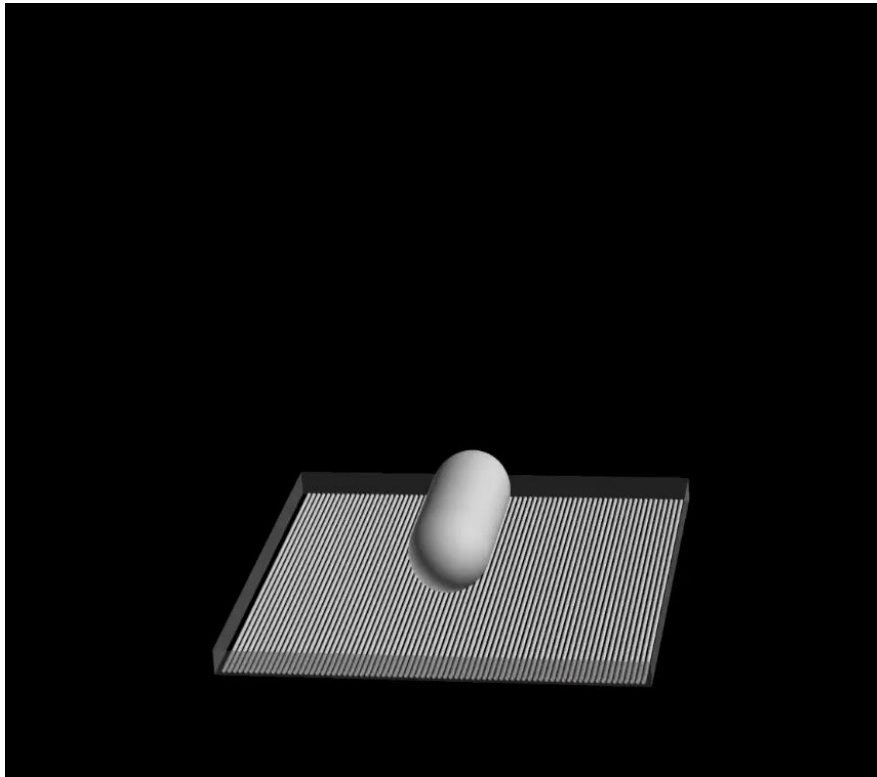


- **GTR#13 T are not always satisfied for  $HRR/A=0.228 \text{ MW/m}^2$  (initial test stage).**
- **GTR#13 T are satisfied for  $HRR/A=1 \text{ MW/m}^2$  (concluded from initial test stage).**

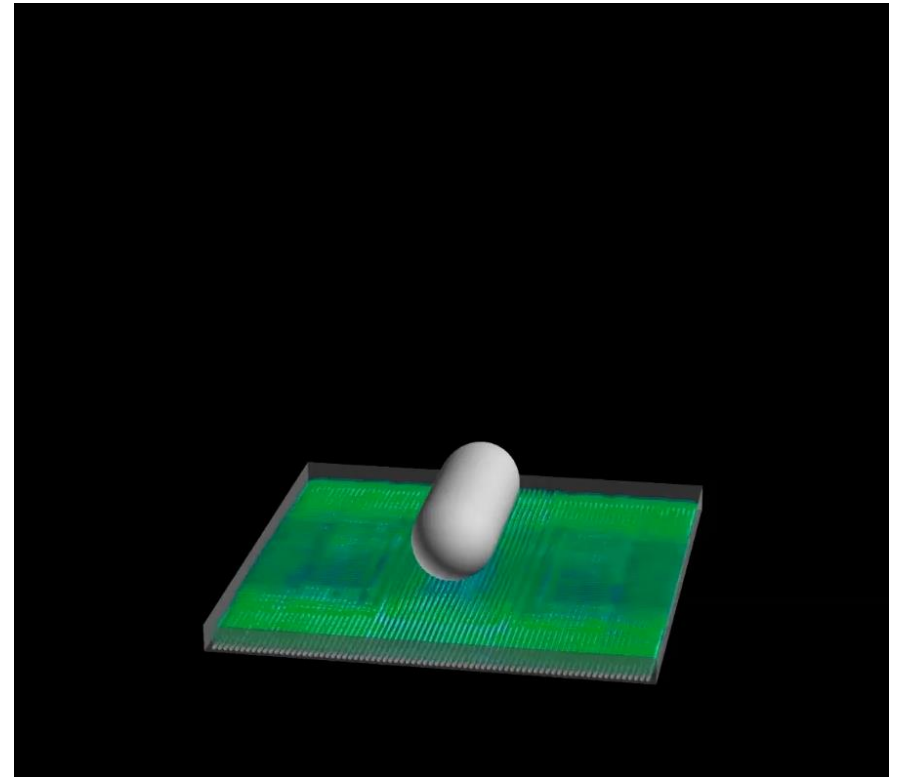
# Pipe burner: wind effect (1.8 m/s)

## Simulation video (temperature)

Case1:  $HRR/A=0.228 \text{ MW/m}^2$



Case 2:  $HRR/A=1 \text{ MW/m}^2$



Temperatures:

 590°C (GTR#13 min required)

 1030°C

# Intermediate remarks (engulfing test)

## Pipe burner

- With no wind, the engulfing fire test with the pipe burner satisfies GTR#13 minimum temperatures at  $HRR/A=0.228 \text{ MW/m}^2$  and  $1 \text{ MW/m}^2$  (similar to blanket burner).
- In wind conditions, the pipe burner reproduces GTR#13 minimum temperatures with  $HRR/A=1 \text{ MW/m}^2$  and not always reproduces temperatures with  $HRR/A=0.228 \text{ MW/m}^2$ .
- Pipe burner is more “wind resistant” compared to blanket burner (flow velocities 1200 mm/s and 3 mm/s respectively!).
- To improve fire test reproducibility the use of pipe burner with  $HRR/A > 1 \text{ MW/m}^2$  can be recommended (in addition to the temperature requirements).

# Concluding remarks

## Engulfing test

- Engulfing fire test must include determination of a tank FRR (time to rupture of tank without TPRD in a fire) as required by first responders in EU HyResponse project.
- Investigated pipe burner performs more “wind resistant” compared to investigated blanket burner.
- “Wind resistant” burner should be designed and used for different wind conditions (only 1.8 m/s is investigated here) to satisfy GTR#13 minimum temperature requirements for engulfing fire test.
- New requirement should be introduced to the temperature control in GTR#13 fire test protocol:  $HRR/A > 1 \text{ MW/m}^2$  should be provided by burner.





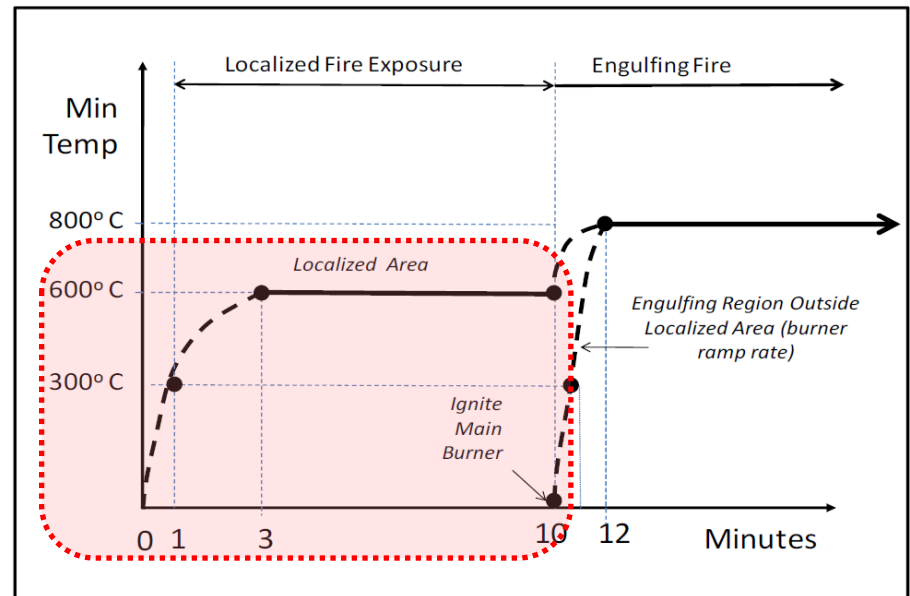
## Part 2. Localised in-situ fire

# GTR#13 temperature requirements

## 6.2.5.1. Fire test (localised + engulfing)

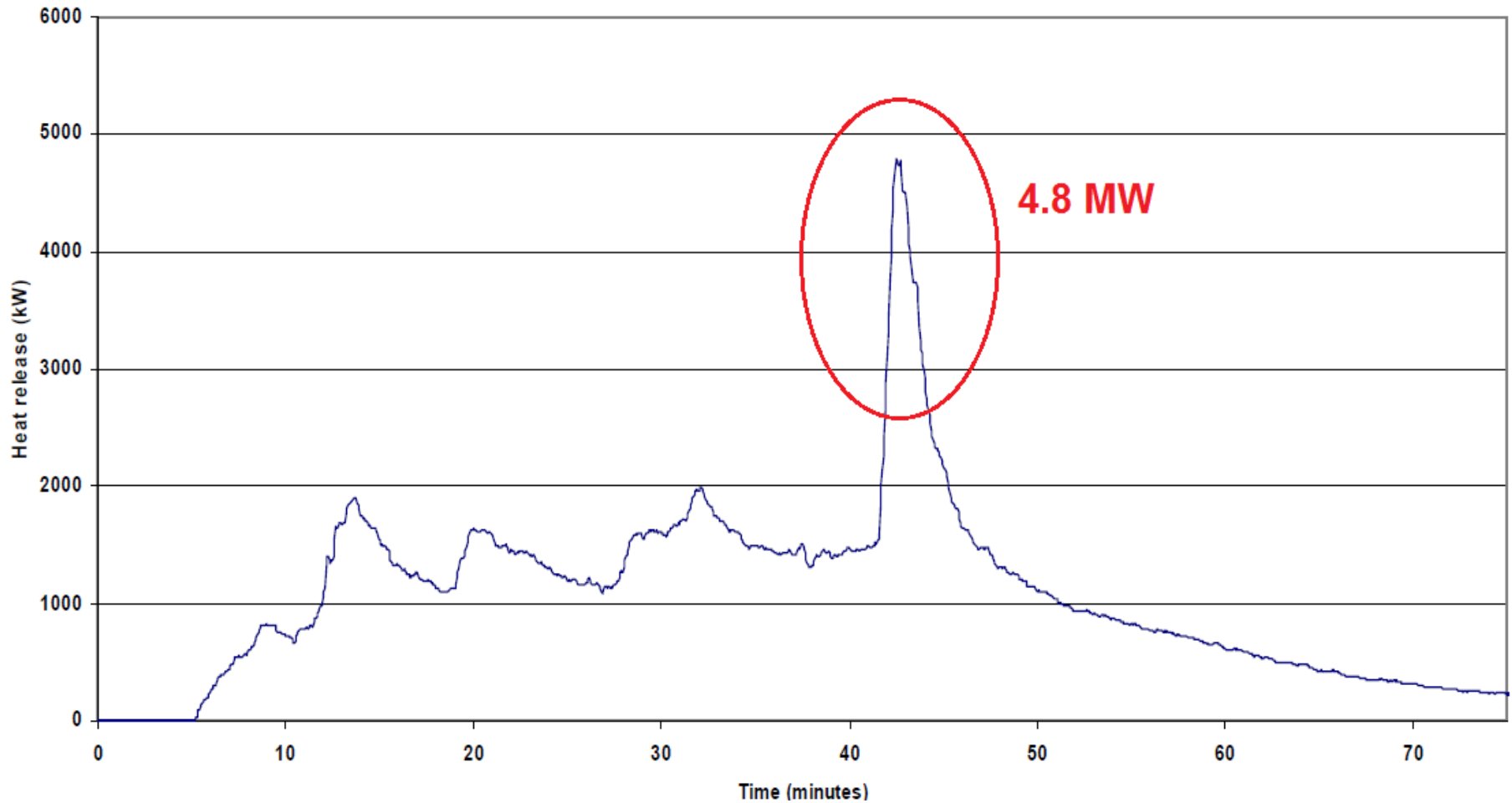
### Localised portion of the fire test:

“...the temperature of the thermocouples in the localized fire area has increased continuously to at least 300 °C within 1 minute of ignition, to at least 600 °C within 3 minutes of ignition, and a temperature of at least 600 °C is maintained for the next 7 minutes ...”



# Reference 1: fuel spill during car fire

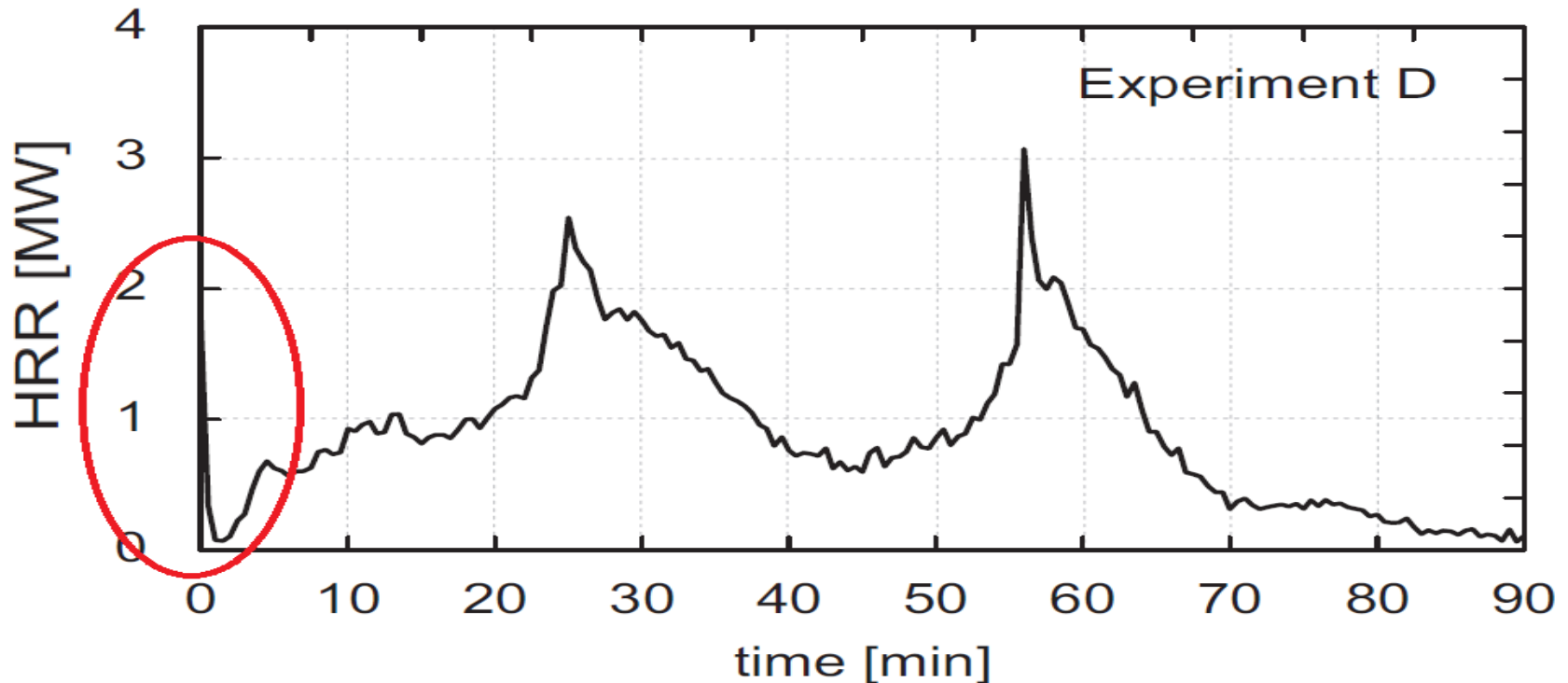
Increase of HRR by  $(4.8 \text{ MW} - 2 \text{ MW}) = 2.8 \text{ MW}$



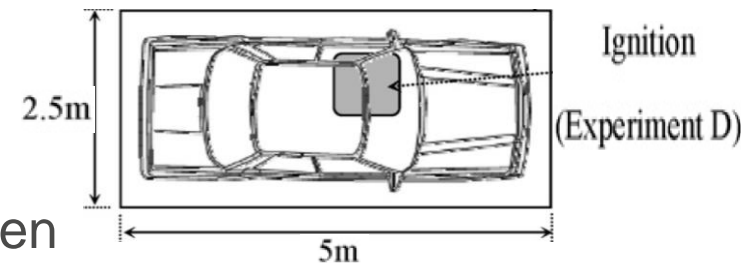
“The 4.8 MW peak is associated with a spillage of fuel”.

# Reference 2: fuel spill in a car

HRR about 1.7 MW from the gasoline fire start



The HRR was more than 1.7MW immediately after ignition of gasoline spill inside a car for about 2-3 min then combustion inside the car was suppressed quickly due to the lack of oxygen (it would give  $3.4 \text{ MW/m}^2$  for  $0.5 \text{ m}^2$  spill).



**Source:** K. Okamoto et al., Burning behaviour of sedan passenger cars, Fire Safety Journal, 44, 2009.

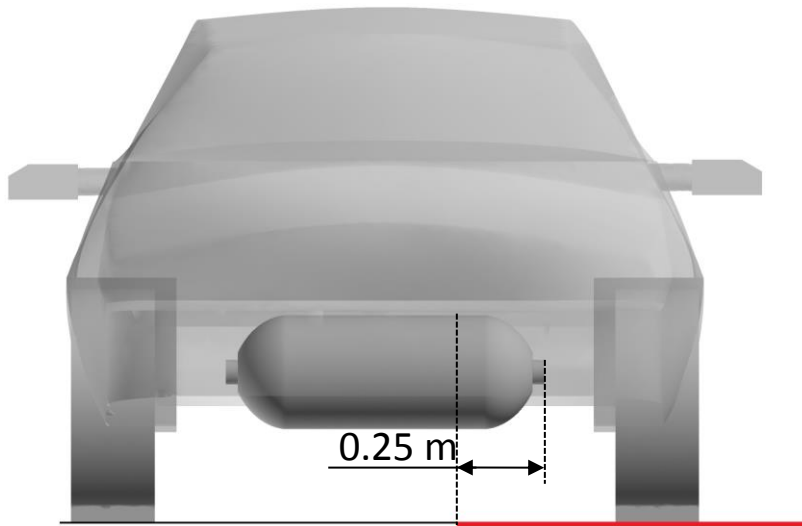
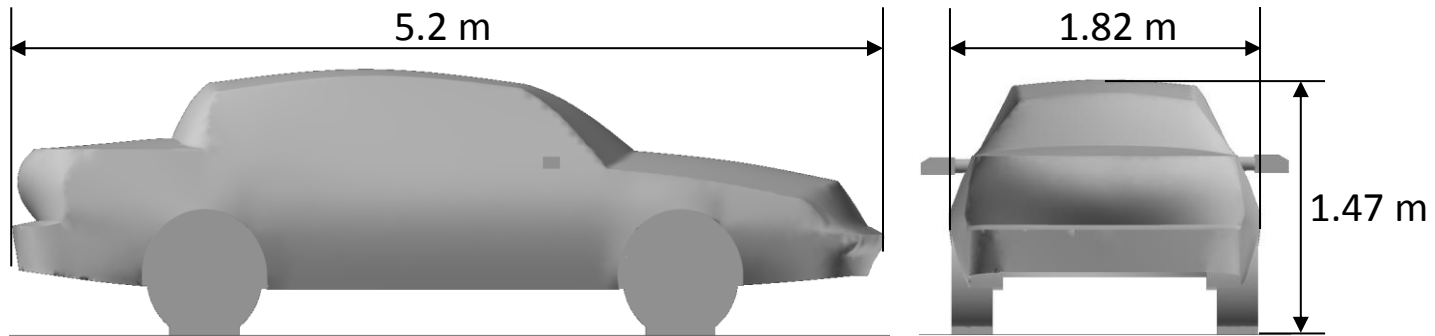
# Four localised fires under a vehicle

Range:  $A=0.2-1.9 \text{ m}^2$ ,  $HRR/A=0.2-2.3 \text{ MW/m}^2$

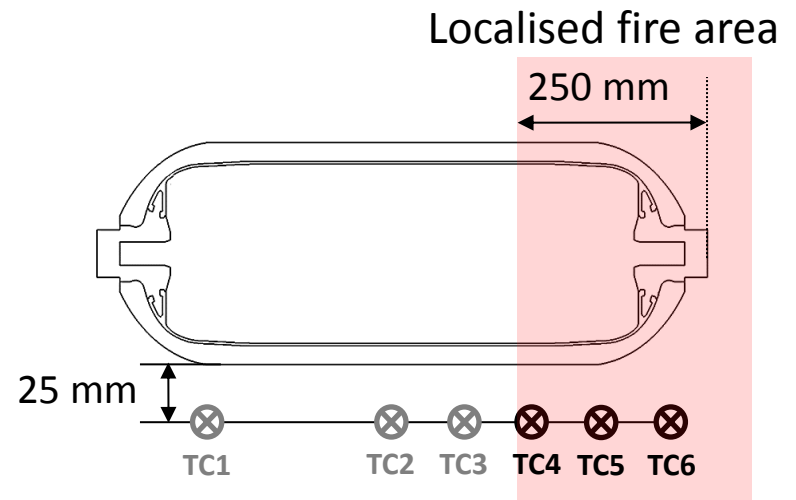
- **Case 1:** *surrogate fuel*, C3H8 equivalent  $\dot{m}=8.2 \text{ g/s}$ .  
Burner  $A=1.9 \text{ m}^2$ ,  $HRR=0.38 \text{ MW}$ :  **$HRR/A=0.2 \text{ MW/m}^2$** .
- **Case 2:** *surrogate fuel*, C3H8  $\dot{m}=41 \text{ g/s}$ .  
Burner  $A=1.9 \text{ m}^2$ ,  $HRR=1.9 \text{ MW}$ :  **$HRR/A=1 \text{ MW/m}^2$** .
- **Case 3:** *diesel*  $\dot{m}=4.72 \text{ g/s}^{(*)}$ , C3H8  $\dot{m}=4.31 \text{ g/s}$ .  
Burner  $A=0.2 \text{ m}^2$ ,  $HRR=0.2 \text{ MW}$ :  **$HRR/A=1 \text{ MW/m}^2$** .
- **Case 4:** *diesel*  $\dot{m}=103 \text{ g/s}^{(*)}$ , C3H8  $\dot{m}=94.5 \text{ g/s}$ .  
Burner  $A=1.9 \text{ m}^2$ ,  $HRR=4.38 \text{ MW}$ :  **$HRR/A=2.3 \text{ MW/m}^2$** .

# Four localised fires under a car

## Car and tank geometry, TCs and fire location



Fire source (No.1, No.2) covers localized area of tank 0.25 m

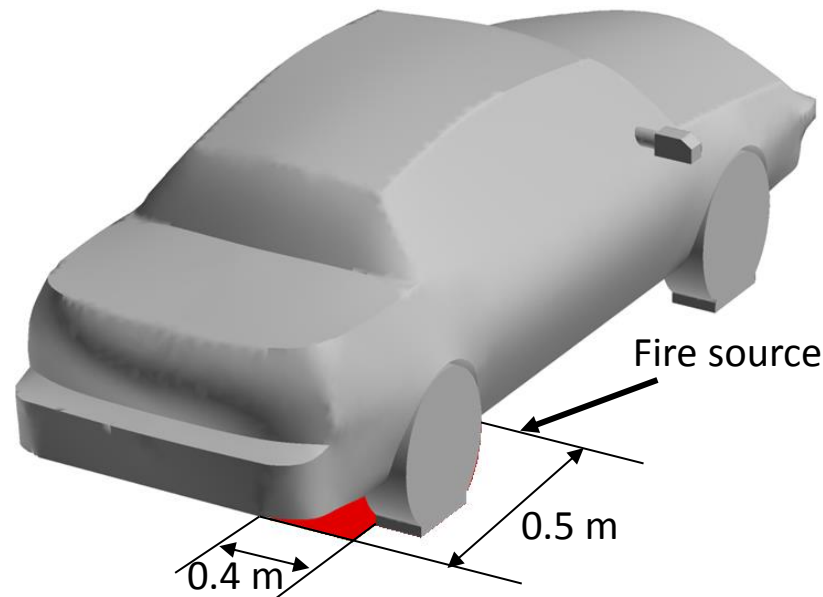


Conjugate heat transfer from fire to 700 bar Type 4 tank (LxD=0.91x0.325 m).

# Localised fire: diesel fire with $A=0.2 \text{ m}^2$

## Case 3

- Fire area  $A=0.2 \text{ m}^2$  (fire source of area No.1), diesel  $\dot{m}=4.72 \text{ g/s}$ .
- Total HRR=0.2 MW;
- Hence,  $\text{HRR}/A=1 \text{ MW/m}^2$ .



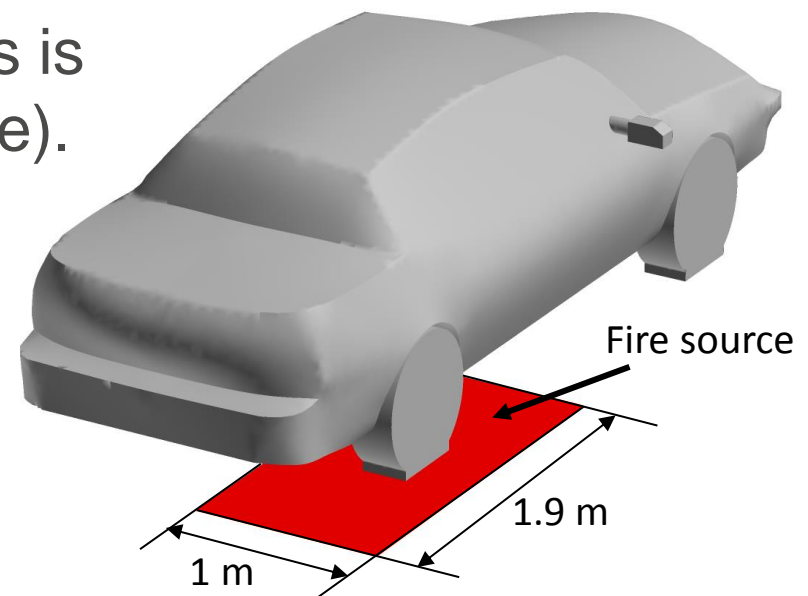
# Localised fire: diesel fire with $A=1.9 \text{ m}^2$

## Case 4

For pool fire of about 1-2 m (localised fire) the fuel burning rate can be taken as quasi-steady value (literature sources).

- Burning rate of diesel for such fire sizes is  $\dot{V}=3.9 \text{ mm/min}$ .
- This is equivalent to  $\dot{m}_A=54.08 \text{ g/m}^2/\text{s}$ .
- Fire area  $A=1.9 \text{ m}^2$  (fire source of area No.2),  $\dot{m}=103 \text{ g/s}$ .
- Total HRR=4.38 MW;
- Thus  $\text{HRR}/A=2.3 \text{ MW/m}^2$  (this is close to References 1-2 above).

**Source:** D. Drysdale, An introduction to fire dynamics, 3rd ed., 2011.



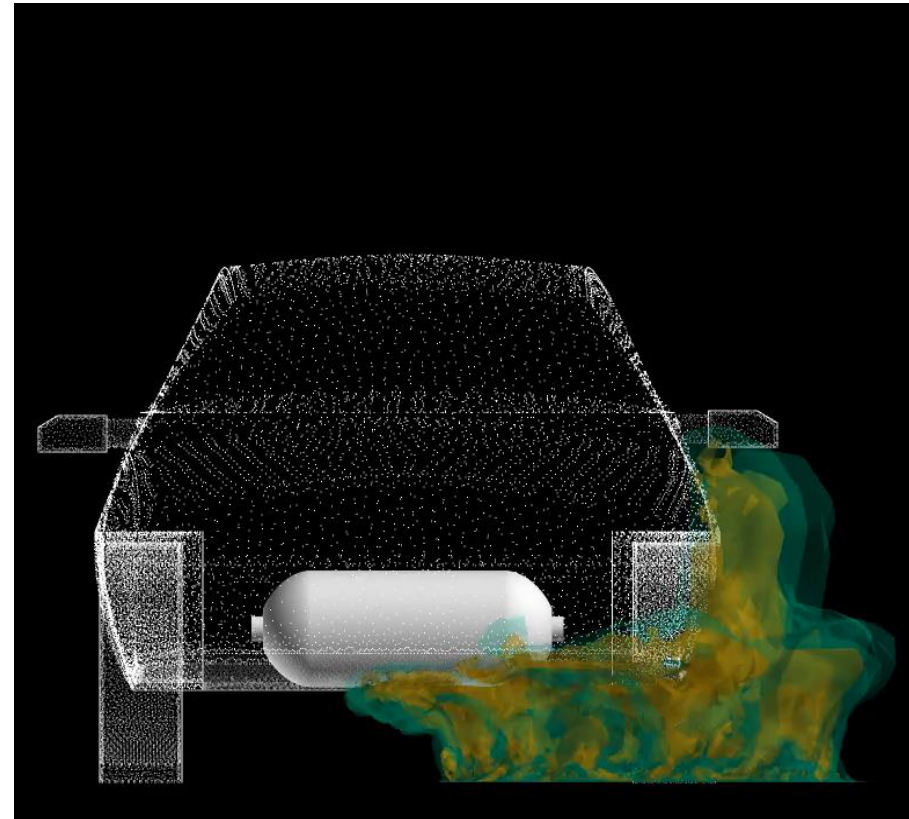
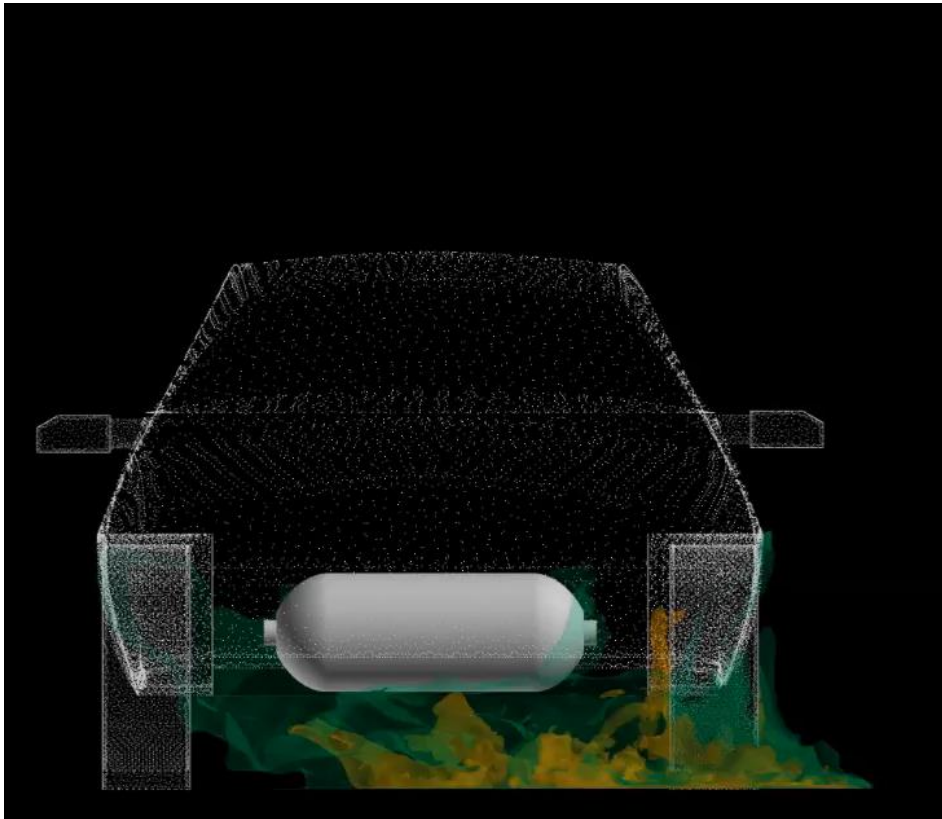


# In-situ fire dynamics: cases 1 and 2

## Video

Case 1:  $\text{HRR}/\text{A}=0.2 \text{ MW}/\text{m}^2$

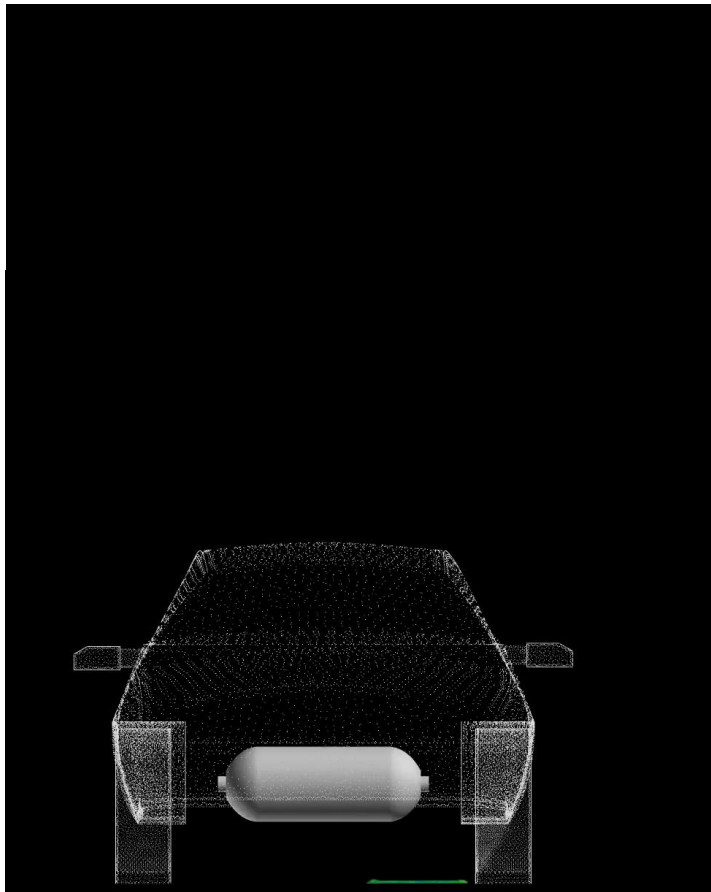
Case 2:  $\text{HRR}/\text{A}=1 \text{ MW}/\text{m}^2$



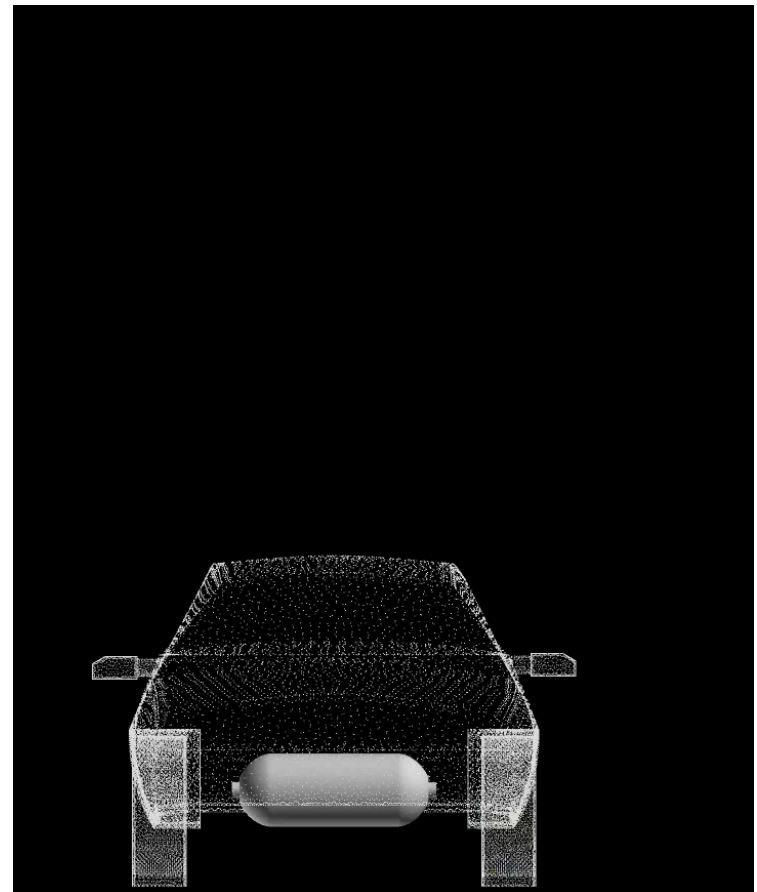
# In-situ fire dynamics: cases 3 and 4

## Video

Case 3:  $HRR/A=1 \text{ MW/m}^2$



Case 4:  $HRR/A=2.3 \text{ MW/m}^2$



 600°C (GTR#13 min required)

 1030°C

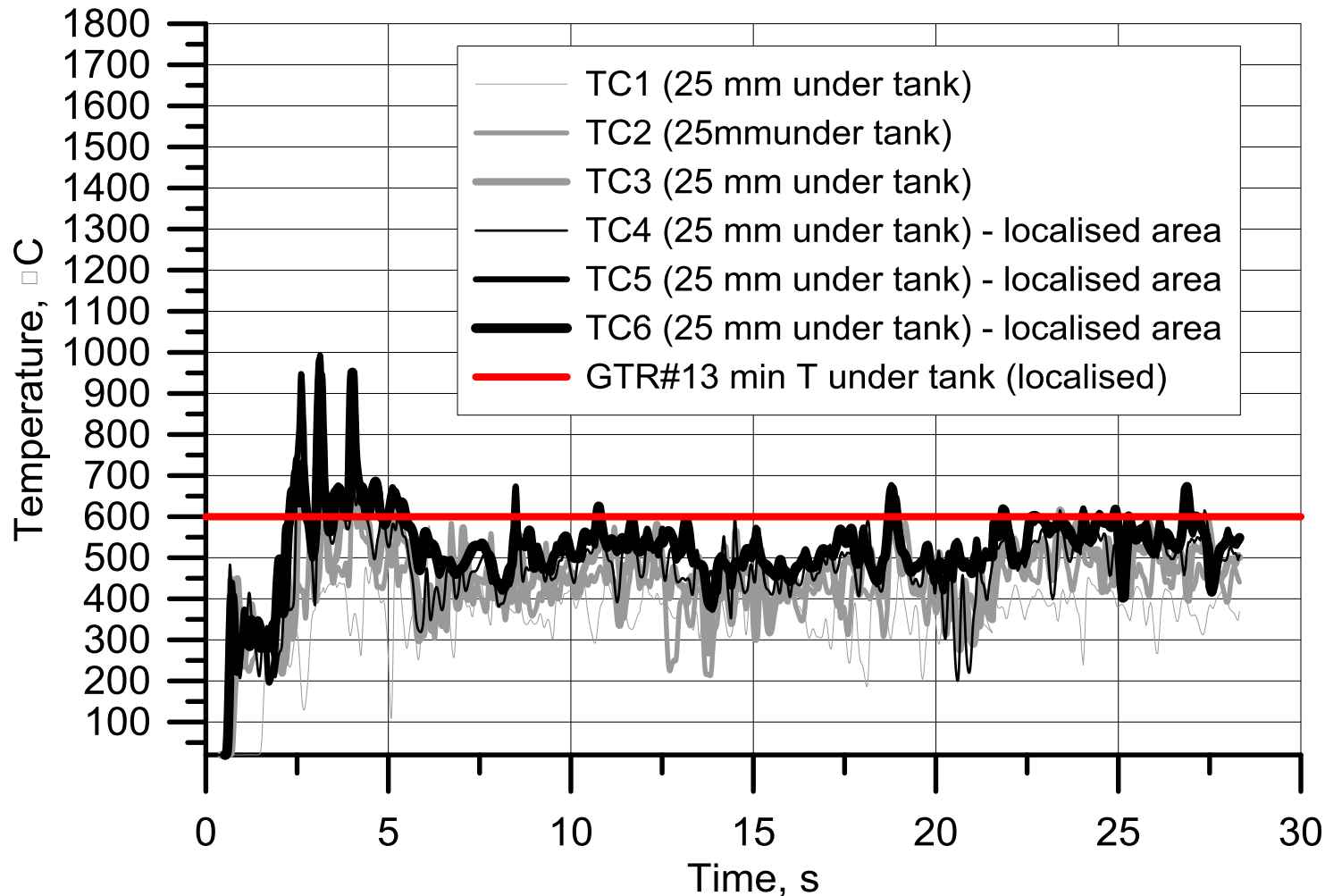
# Four localised fires under a car

## Questions to answer

- Would the range of localised fires with different specific heat release rate,  $HRR/A$ , from  $0.2 \text{ MW/m}^2$  to  $2.3 \text{ MW/m}^2$  provide agreements with GTR#13 temperature requirements?
- How different will be heat flux to a tank from a fire for different  $HRR/A$ ?
- If GTR#13 fire test temperature requirements are fulfilled, but the heat flux to the tank is different – would this affect the fire resistance rating (FRR) of a tank (time to rupture of a tank without or failed to be initiated TPRD, e.g. being blocked during accident)?

# In-situ fire: $HRR/A=0.2 \text{ MW/m}^2$

## Temperature under tank (simulations): Case1

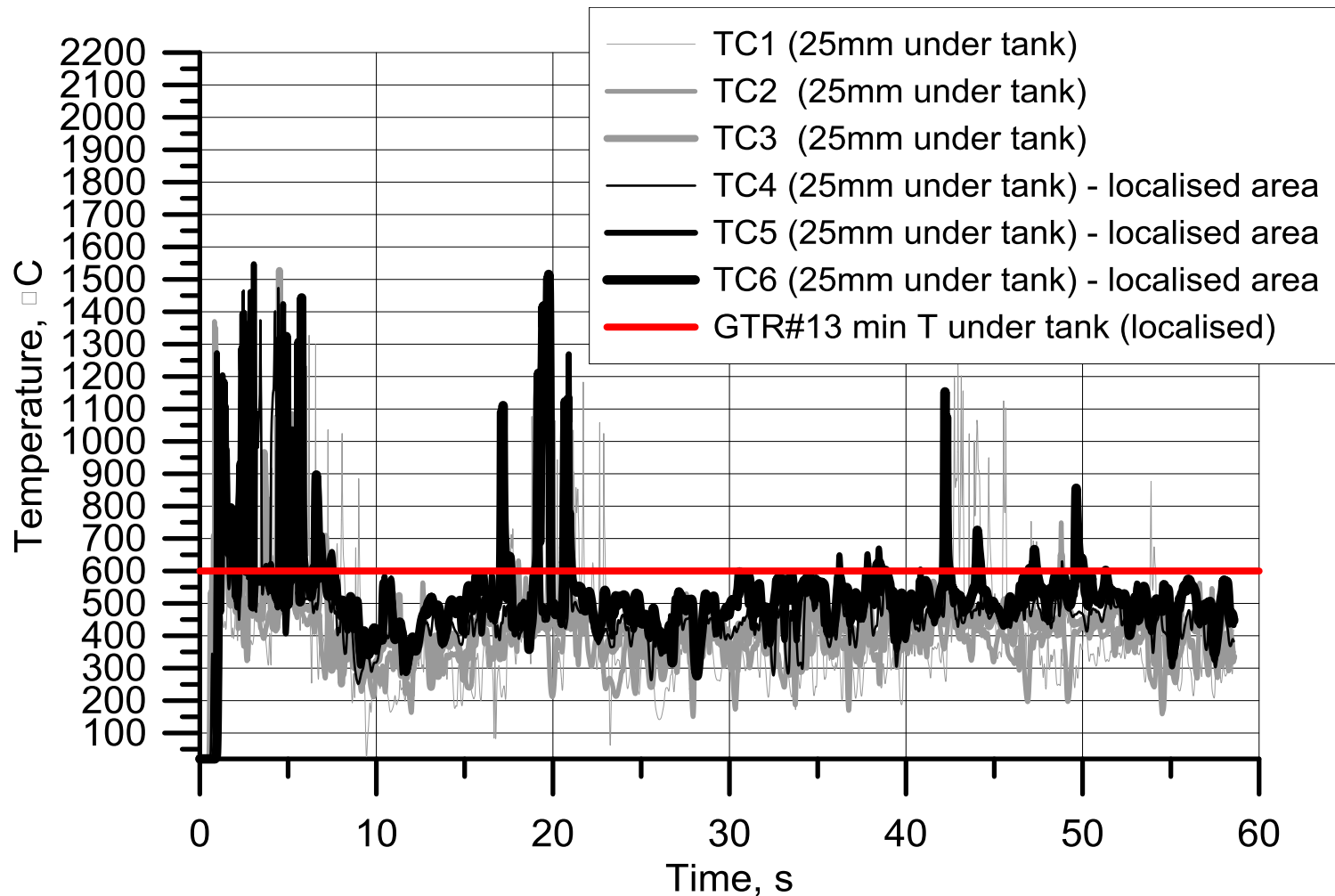


**GTR#13 minimum T requirements are not satisfied for in-situ test (!)**

FRR of the tank for  $HRR/A= 0.2 \text{ MW/m}^2$  (surrogate fuel) is 24 min.

# In-situ fire: $HRR/A=1 \text{ MW/m}^2$

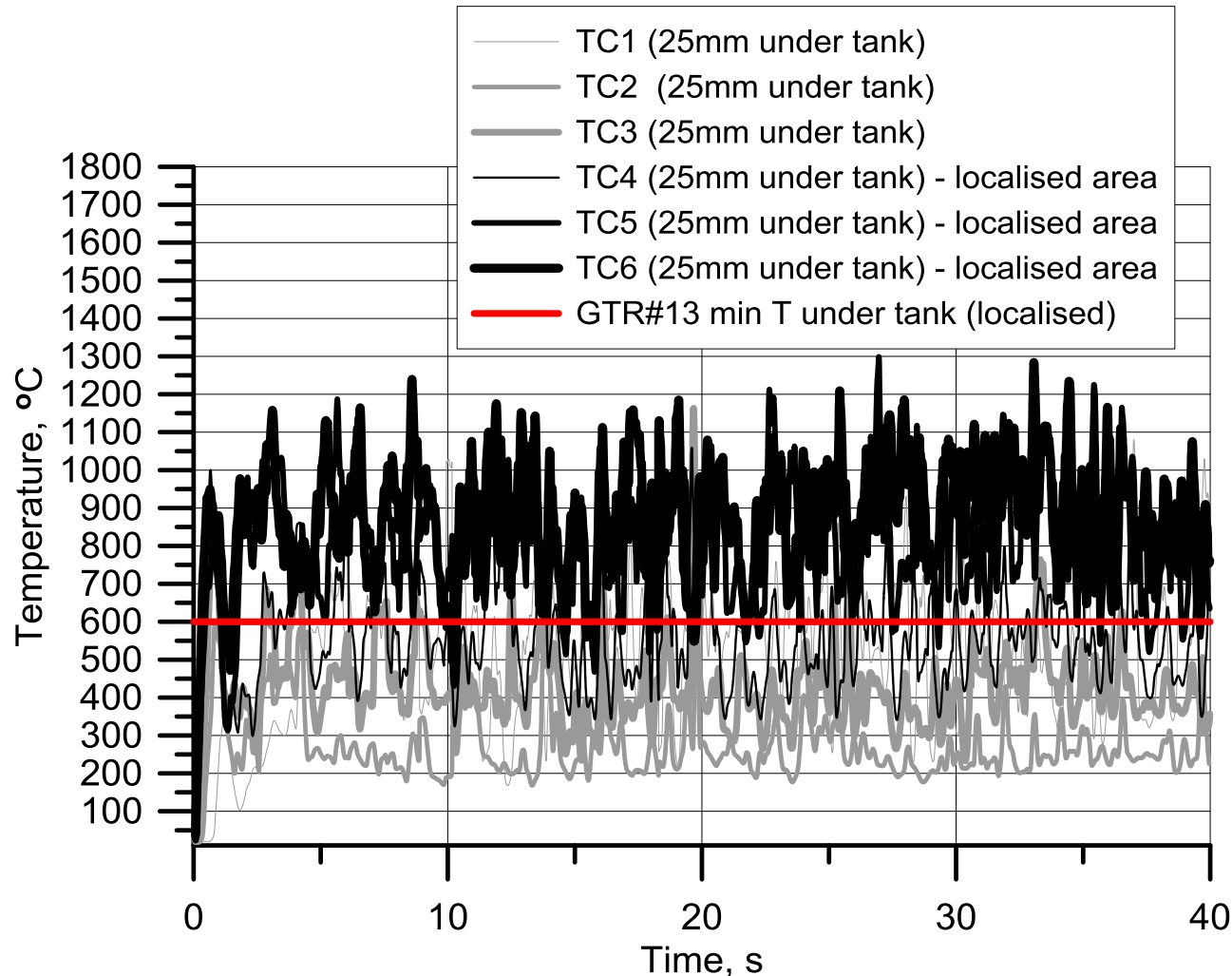
## Temperature under tank (simulations): Case 2



**GTR#13 min T requirements are not always satisfied ( $A=1.9 \text{ m}^2$ ).**  
FRR of the tank for this  $HRR/A=1 \text{ MW/m}^2$  (surrogate fuel) is 6 min.

# In-situ fire: $HRR/A=1 \text{ MW/m}^2$

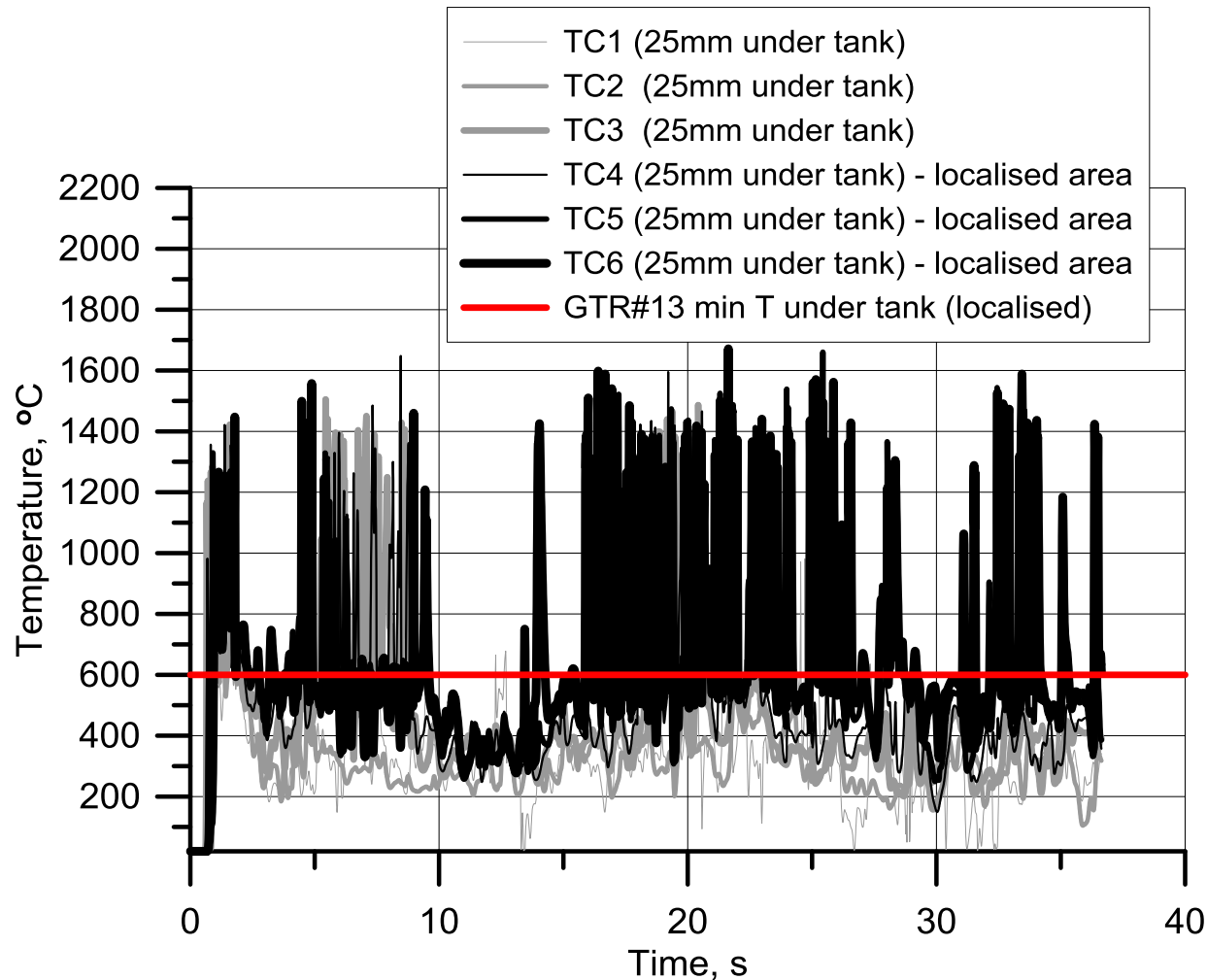
## Temperature under tank (simulations): Case 3



**GTR#13 minimum T requirements are satisfied ( $A=0.2 \text{ m}^2$ ).**  
**FRR of the tank for this  $HRR/A$  (diesel) is 5 min 20 s.**

# In-situ fire: $HRR/A=2.3 \text{ MW/m}^2$

## Temperature under tank (simulations): Case 4

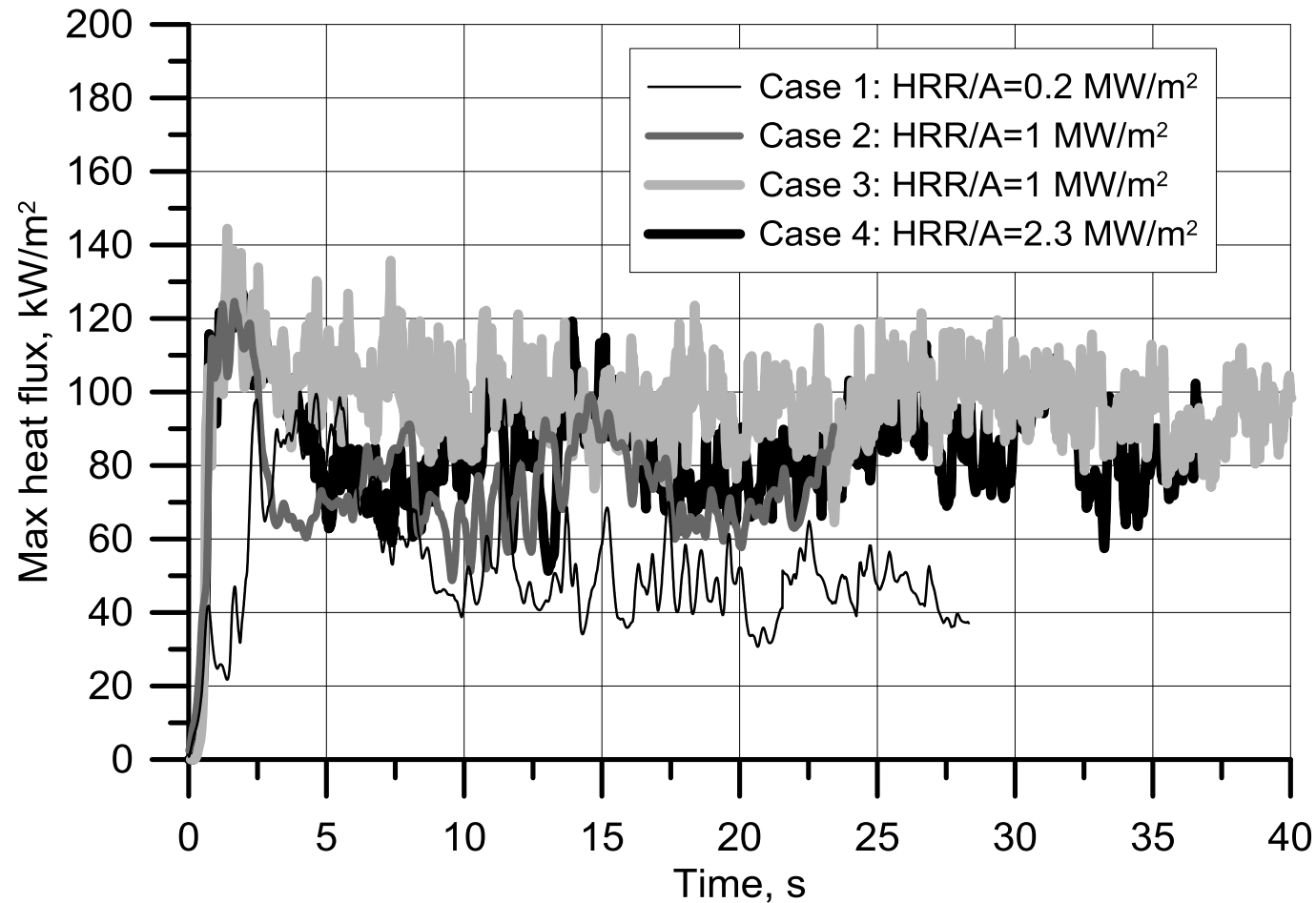


**GTR#13 minimum T requirements are satisfied.**

**FRR of the tank for this HRR/A (diesel) is 5 min 50 s.**

# Heat flux to tank in four in-situ fires

## Cases 1-4



Heat flux to the tank is similar for Cases 2-4:  $HRR/A \geq 1$  MW/m<sup>2</sup>.  
Heat flux for Case 1 with  $HRR/A=0.2$  MW/m<sup>2</sup> is noticeably less.

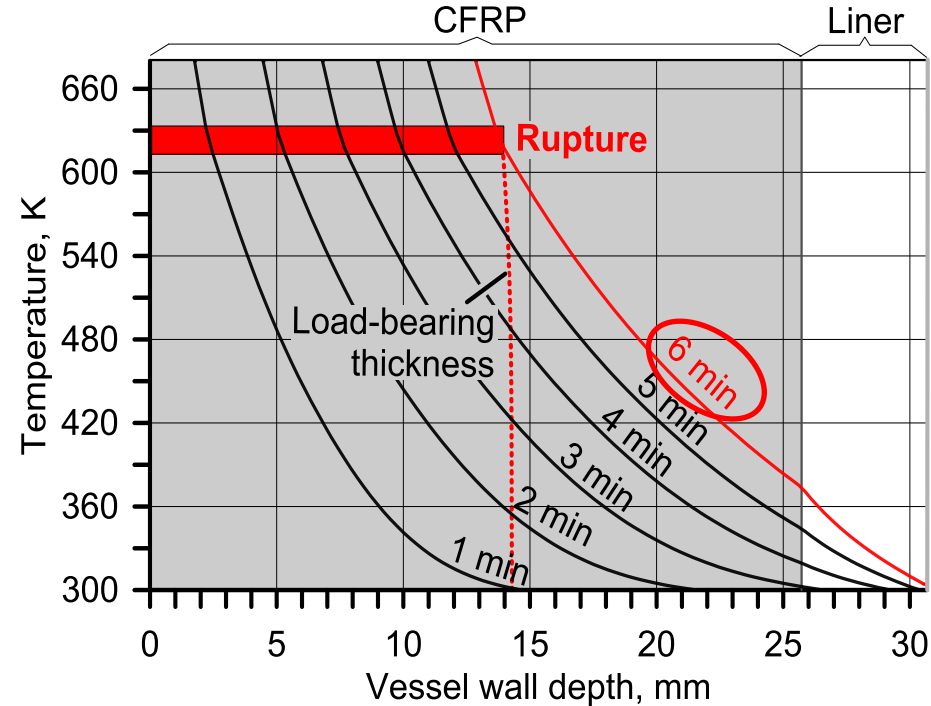
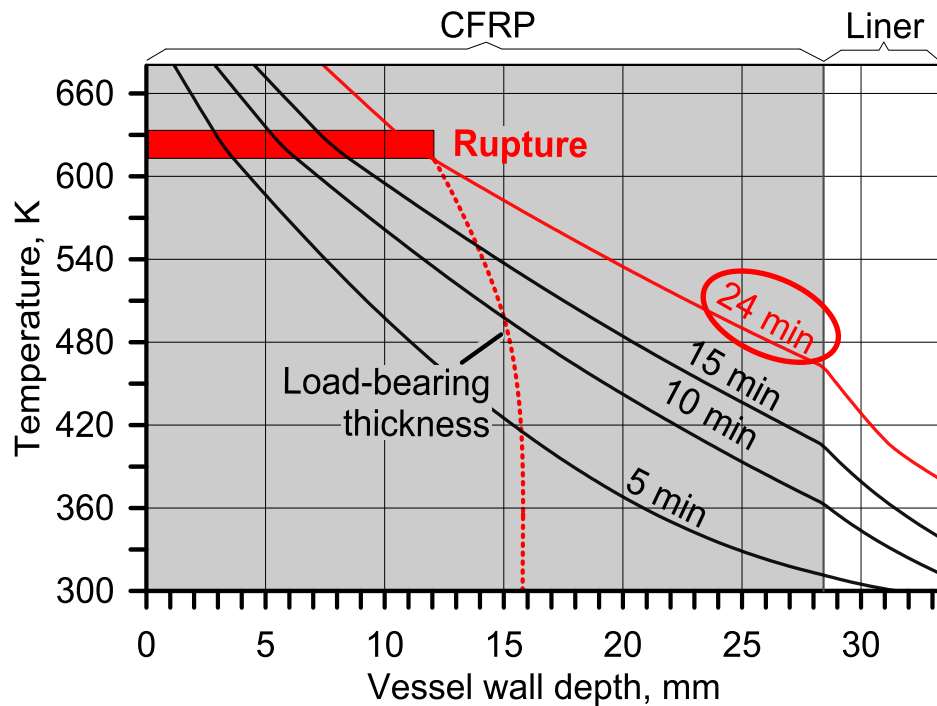


# Localised fire under a car: FRR (1/2)

## 700 bar, Type 4 tank (0.91x0.325 m)

Case1:  $HRR/A=0.2 \text{ MW/m}^2$

Case2:  $HRR/A=1 \text{ MW/m}^2$

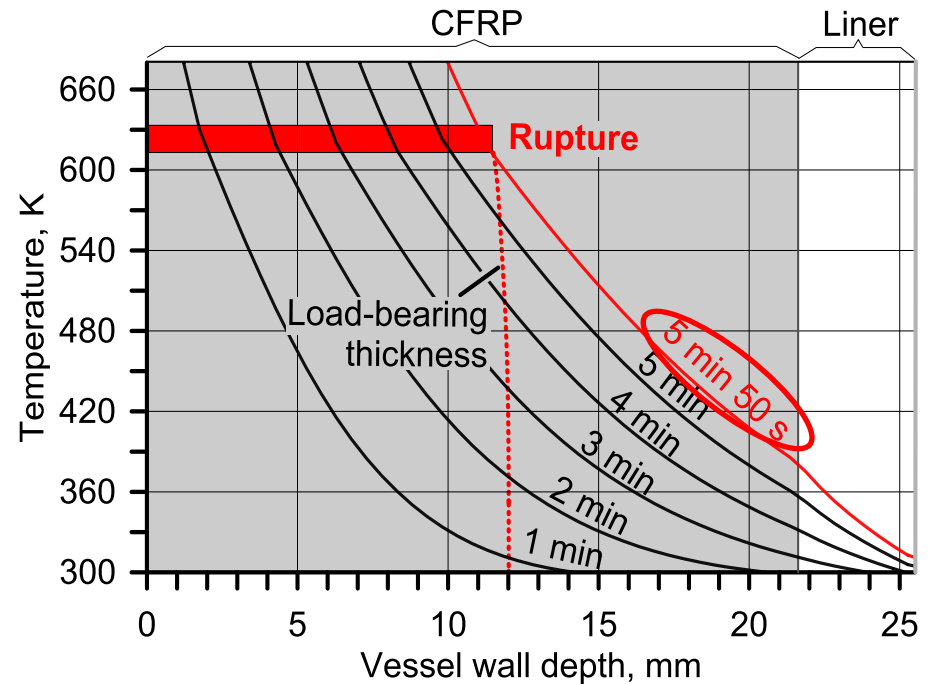
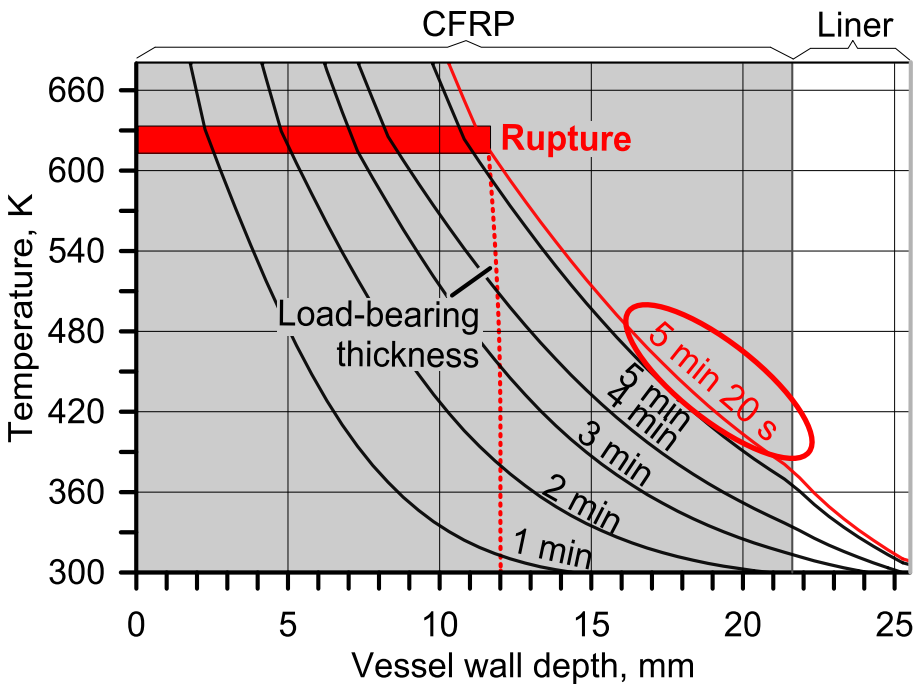


# Localised fire under a car: FRR (2/2)

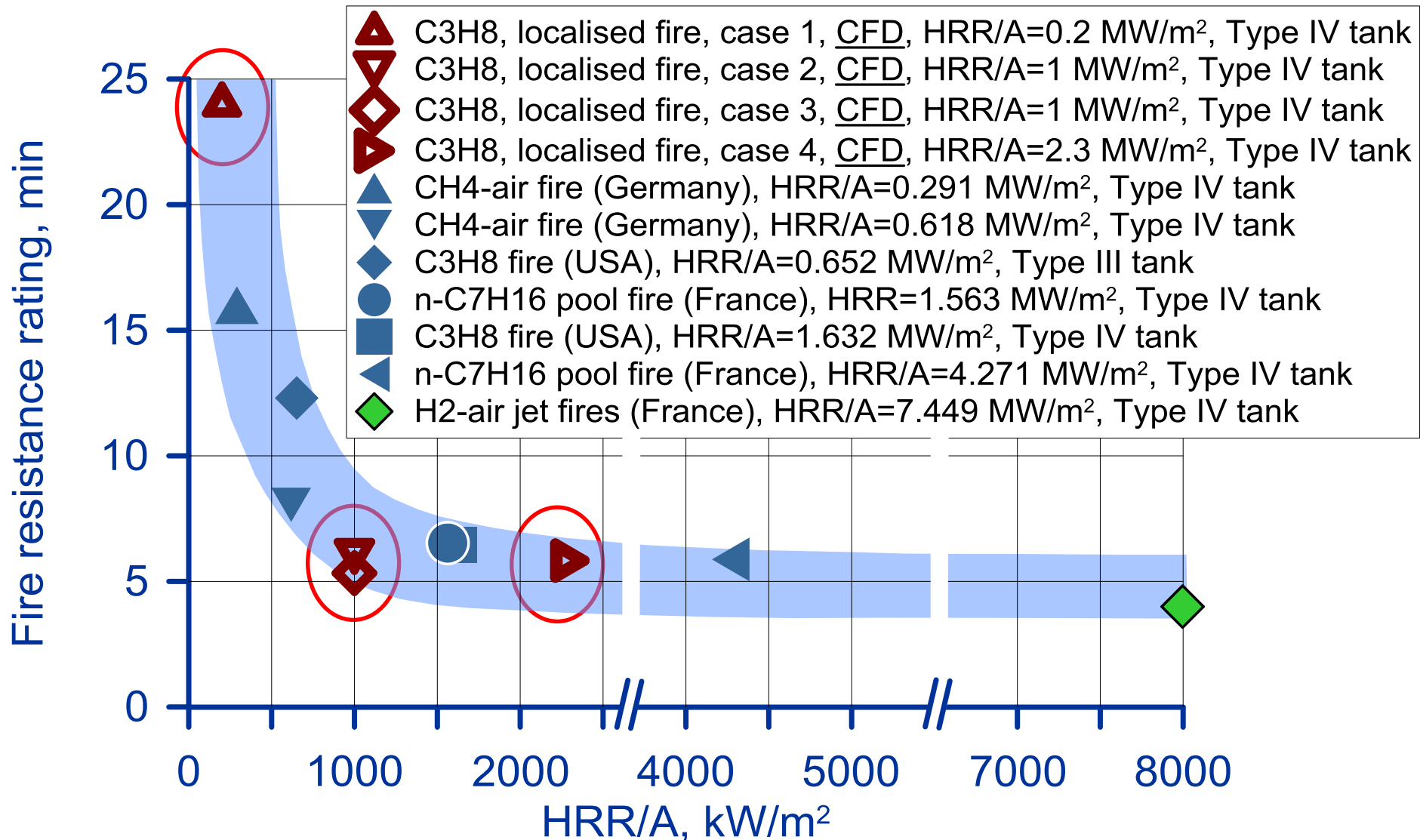
## 700 bar, Type 4 tank (0.91x0.325 m)

Case 3:  $HRR/A=1 \text{ MW/m}^2$

Case 4:  $HRR/A=2.3 \text{ MW/m}^2$



# FRR dependence on HRR/A



Saturation of FRR with HRR/A after 1 MW/m²

# Three in-situ fire questions answered

- Would the range of localised fires with different specific heat release rate, HRR/A, from 0.2 MW/m<sup>2</sup> to 2.3 MW/m<sup>2</sup> provide agreement with GTR#13 temperature requirements? **Answer: No!**
- How different will be heat flux to a tank from a fire for different HRR/A? **Answer:  $\dot{q}''=50$  kW/m<sup>2</sup> (HRR/A=0.2 MW/m<sup>2</sup>);  $\dot{q}''=90$  kW/m<sup>2</sup> (HRR/A>1 MW/m<sup>2</sup>)**
- If GTR#13 fire test temperature requirements are fulfilled, but the heat flux to the tank is different – would this affect the fire resistance rating (FRR) of a tank (time to rupture of a tank without or failed to be initiated TPRD, e.g. being blocked during accident)? **Answer: Yes! For HRR/A=0.2 MW/m<sup>2</sup>, FRR=19 min. For HRR/A=1.0-2.3 MW/m<sup>2</sup>, FRR=5.3-6.0 min**

# Concluding remarks

## Localised test

- Carried out research demonstrated that in-situ localised fire test is more appropriate for assessment of TPRD performance.
- GTR#13 localised fire test minimum temperature requirements cannot be realised for in-situ fire test with  $HRR/A < 1 \text{ MW/m}^2$ .
- GTR#13 localised fire test minimum temperature requirements must be added by a requirement of  $HRR/A > 1 \text{ MW/m}^2$  in a burner.
- Similar to engulfing fire, the increase of  $HRR/A$  in localised fire resulted in the increase of heat flux to a tank and the decrease of FRR (with clear “saturation” of FRR at  $HRR/A > 1 \text{ MW/m}^2$ ).
- FRR in localised fire (time to rupture on tank without TPRD in a fire) obey the same “saturation curve” as FRR in engulfing fire.
- FRR should be included into GTR#13 fire test protocols to inform responders to develop intervention strategies and tactics.

# THANK YOU

